

NUREGCR5658



NUREG/CR-5658
PNL-7513
1A, 1B

FPFP_2: A Code for Following Airborne Fission Products in Generic Nuclear Plant Flow Paths

Manuscript Completed: February 1991
Date Published: March 1991

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Prepared for
Division of Safety Issue Resolution
Office of Nuclear Regulatory Research
U.S. Nuclear Regulatory Commission
Washington, DC 20555
NRC FIN B2929

REPRODUCED BY: **NTIS**
U.S. Department of Commerce
National Technical Information Service
Springfield, Virginia 22161

ABSTRACT

This report describes the technical bases and use of the computer code FPF₂ (Fission Product Flow Paths). FPF₂ was developed to estimate the concentrations and flow rates of airborne fission products along a generic flow path following a transient or puff source of fission products at the beginning of the flow path. This report serves as a user's guide for FPF₂. A complete code description, code operating instructions, code listing, and an example of the use of FPF₂ support the use of the code.

SUMMARY

The software package FFP_2 enables the user to follow fission product noble gases, molecular iodine, and particles along a flow path from a source to an end point. The user constructs the flow path consisting of a series arrangement of rooms, ducts, filters, or flow resistances. Parallel flow paths can be analyzed by studying each series element independently and superimposing the individual results. The user must supply flow path flow rates and fission product concentrations at the source as functions of time during the transient event and, as an option, supply the initial source term as a puff release in the farthest upstream room. FFP_2 calculates the fission product concentrations and flow rates between or within the flow path components. These concentrations reflect dilution and transient time, deposition processes (iodine and particles), spray washout (particles), and filtration (iodine and particles) that fission products experience along the flow path.

CONTENTS

ABSTRACT	iii
SUMMARY	v
1.0 INTRODUCTION	1
2.0 TECHNICAL BASES	3
2.1 FLOW PATH COMPONENTS	3
2.1.1 Rooms	3
2.1.2 Ducts	3
2.1.3 Filters	4
2.1.4 Flow Resistances	4
2.2 FISSION PRODUCT DEPOSITION	4
2.2.1 Iodine Vapor	4
2.2.2 Particles	6
3.0 CODE DESCRIPTION	7
3.1 CODE ORGANIZATION	7
3.2 SUBROUTINES	8
4.0 CODE OPERATION	9
4.1 BLDINPT2	9
4.1.1 Puff Release and Other Variables	9
4.1.2 Plant Variables	9
4.1.3 Other Fission Product Sources	9
4.1.4 Gas Variables	10
4.1.5 Spray Variables	10
4.2 OUTPUT DESCRIPTION	10
4.3 SAMPLE CASE	10
5.0 REFERENCES	15

APPENDIX A - FPDF_2 LISTING	A.1
APPENDIX B - SAMPLE CASE INPUT AND OUTPUT FILES	B.1
APPENDIX C - BLANK BLDINPT2 FORMS	C.1
APPENDIX D - BLDINPT2 LISTING	D.1

FIGURES

1	Schematic Diagram of FPPF_2 Showing Components and Information Flow	7
2	Sample Case Flow Path Showing Nodes, Components (Spaces), and Flow Rates	12
3	Concentration of Fission Products in Sample Case Space 4 as a Function of Time as Calculated by FPPF	13

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1. The first step in the process of identifying a problem is to recognize that a problem exists. This is often done by comparing current performance against a desired state or goal. For example, a manager might notice that sales are declining or that customer satisfaction is low. Once a problem is identified, the next step is to define it clearly and specifically. This involves determining the scope of the problem, its causes, and its effects. A clear definition of the problem is essential for developing an effective solution. The third step is to analyze the problem and its underlying causes. This involves gathering relevant information, identifying key factors, and understanding the relationships between them. A thorough analysis helps to pinpoint the root cause of the problem, which is crucial for developing a targeted solution. The fourth step is to generate potential solutions. This involves brainstorming ideas, consulting with others, and exploring different approaches. It is important to consider a range of options and to evaluate their potential benefits and risks. The fifth and final step is to select and implement a solution. This involves choosing the most appropriate solution, developing a plan of action, and putting it into practice. It is essential to monitor the progress of the solution and to make adjustments as needed to ensure that the problem is effectively resolved.

1.0 INTRODUCTION

In order to assure that a nuclear power plant control room remains habitable during certain types of postulated accidents, Pacific Northwest Laboratory (PNL) has undertaken a special study for the U.S. Nuclear Regulatory Commission. The purpose of this study is to develop software that can aid in the analyses of control room habitability during accidents in which airborne fission products could challenge internal air pathways to the control room. PNL has completed an initial version (FPFP) and final version (FPFP_2) of a software package that can estimate the unsteady-state invasion of quantities of fission products into the control room or any other destination within the nuclear plant via generic internal flow paths.

This report consists of three parts: Section 2.0, Technical Bases, describes the flow path components and mechanisms of natural fission product deposition; Section 3.0, FPFP_2 Code Description, describes code organization and the functions of the subroutines; and Section 4.0, Code Operation, discusses details of input requirements, code output, and a sample case demonstration. The appendices consist of an FPFP_2 Fortran code listing, a listing of a code for building input files, forms for building input files, and the sample case input and output files.

2.0 TECHNICAL BASES

This section discusses the technical aspects of the flow path components and the fission product deposition mechanisms. FFPF_2 allows the user to analyze only one flow path at a time, even if there are many parallel and cross-linked paths between the source and final sink of fission products. The user can analyze a complex network where the gas flow rates are known in all parts of this network by adding up all fission product concentrations and flow rates from each path analysis. FFPF_2 assumes that the fission products do not interact and that all deposition rates are linearly dependent on fission product airborne concentrations.

2.1 FLOW PATH COMPONENTS (SPACES)

The flow path components (referred to as spaces in the code) are designed to carry out various functions. A generic flow path in FFPF_2 is considered to be a series of N nodes and N-1 components (or spaces). The nodes are merely flow splitters or link points to other flow paths. Please see the sample case described in Section 4.3 to see the relationship between nodes and components. The most important components appear to be rooms, ducts, filters, and flow resistances.

2.1.1 Rooms

FFPF_2 assumes that the gases entering a room become well mixed in the room. Gases leave the room at the well-mixed concentration. Rooms not only dilute the incoming gases, they can remove iodine by surface deposition, particles by gravitational settling, and particles by liquid sprays. Spray washout of iodine is not modeled here.

2.1.2 Ducts

A duct is a flow path component where gases enter at one end of a long, constant cross-section system and proceed to an exit. There might be situations where it is difficult to decide whether a component is a room or duct. Situations where a duct has many turns or cross-section changes will require engineering judgment to arrive at an equivalent constant cross-section duct. Equivalent cross sections will be further discussed in Section 4.1.

FFPF_2 assumes that plug flow exists in a duct. This assumption precludes any diffusion in the flow direction and simplifies the FFPF_2 program. Iodine and particles are allowed to deposit on all surfaces and upward-facing surfaces, respectively. Turbulent diffusion, diffusiophoresis, thermophoresis, and Brownian diffusion of particles are not modeled in FFPF_2.

2.1.3 Filters

Gases passing through a filter experience some removal (decontamination) of fission products. FFP_2 requires that the decontamination factors (DFs) be supplied by the user. Typical DFs are 2000 for particles, 20 for iodine and 1.0 for noble gases.

2.1.4 Flow Resistances

A flow resistance is a convenience for adjusting flow rates between two nodes. FFP_2 treats flow resistance like a filter with all DFs = 1.

2.2 FISSION PRODUCT DEPOSITION

All fission products that can be removed by natural deposition processes are either vapor molecules or fine particles. Organic iodides are considered to be inert gases (like the noble gases), except when they pass through certain absorbers. Iodine vapors (as HI or I₂) are treated as though they were all I₂. Therefore, any exposed surface will be considered as a deposition surface for I₂. Since most well-aged accident aerosol particles are greater than 0.1 micron diameter (Gieseke et al. 1984; Denning et al. 1986) and since accident flow rates leading to control rooms are anticipated to be close to normal duct flow values (i.e., slow), only gravity settling is considered as a removal mechanism apart from filtration.

If a user would like to consider high flow-rate turbulent deposition, that mechanism could be easily added to the code. Diffusiophoretic and thermophoretic deposition mechanisms could be added, but these would require supporting heat transfer and condensation analyses as well.

2.2.1 Iodine Vapor

Iodine vapor reaches deposition surfaces through diffusion through a boundary layer. The deposition velocity (k, ft/min) is obtained from correlations for heat transfer coefficients using the Chilton-Colburn analogy for mass transfer coefficients (Bird, Stewart, and Lightfoot 1960). The Sherwood number (Sh) becomes a function of the Schmidt number (Sc), the Reynolds number (Re), and the friction factor (f):

$$Sh = Sc^{1/3} Re f/2 .$$

For turbulent duct flow, $f = 0.0791/Re^{1/4}$. Other definitions are

$$Sh = kd/D$$

$$Sc = \mu/rD$$

$$Re = rDv/\mu$$

$$r = \text{air density}$$

μ = air viscosity

v = air velocity

$d = 4Rh$

Rh = hydraulic radius

D = iodine diffusivity.

Because the above relationships do not account for surface roughness and bends in ducts, k values will be conservatively low. Values for k will also be conservative when these equations are used to estimate k in rooms. After introducing the deposition velocity for mass transfer, we now examine how it is used.

The differential equation for fission product concentration (c) in a well-mixed room is

$$V(dc/dt) = F_i c_i - (F_o + kA)c$$

where

V = room volume

F_i = actual inlet flow rate

c_i = inlet concentration

F_o = actual outlet flow rate

A = room surface area.

The partial differential equation for concentration in a duct along the x (flow) direction (neglecting diffusion) is

$$\partial c / \partial t = -v \partial c / \partial x - kPc / A_x$$

where

A_x = cross-sectional area

P = perimeter of A_x .

The above two differential equations are solved using a series of time steps over the duration of the transient accident. The noble gases and organic iodides follow the same equations except that $k = 0$.

The equations above assume that the I_2 vapor finds a deposition surface that readily adsorbs the iodine without reentrainment. Therefore, iodine deposition calculated by FFP2 is an upper-bound value. This ideal situation is probably realistic for clean metallic and painted surfaces. However, certain materials can become saturated and reentrain iodine in the presence of

lower I_2 concentrations than the maximum observed during the accident. This reentrainment behavior is material-specific and cannot be easily generalized. The user of FPPF_2 should be aware that iodine can significantly reentrain in the days following deposition. [See Unrein et al. (1985) and Widner et al. (1985) for specific data where iodine reentrainment rates as high as 10^{-5} s^{-1} have been observed.] The user should not include surfaces in the area A for iodine deposition that cannot adsorb the iodine.

2.2.2 Particles

Particles can deposit on surfaces by a number of mechanisms. These are Brownian diffusion, gravity settling, electrophoresis, thermophoresis, diffusio-phoresis, turbulent deposition, inertial impaction, and interception. For typical well-aged nuclear-accident-generated aerosols, with little water vapor present in the gas (i.e., no condensation on walls or particles), with small gas-to-wall temperature gradients, and with velocities that are not excessive, gravity becomes the dominant deposition mechanism. FPPF_2 uses gravity settling as the only particle deposition mechanism, and because the aerosols are well aged, particle agglomeration is ignored.

The differential equations in Section 2.2.1 hold for particle settling with the following changes: k becomes the particle settling velocity, A becomes $A(\text{floor})$, and P becomes duct width.

The equations for deposition velocities have been established in other documents (Owczarski, Schreck, and Winegardner 1985). These velocities are a strong function of particle diameter and a less strong function of particle density. FPPF_2 represents the nuclear aerosol at its source as having an aerodynamic mass median diameter (ammd) of $1 \mu\text{m}$ with a geometric standard deviation of 2. The aerosol particles are distributed into bins of five discrete particle sizes. FPPF_2 allows the user to apply a multiplier to the ammd value. The particle size distribution above is typical of well-aged aerosols found by calculation in severe reactor accidents analyses (Gieseke et al. 1984; Denning et al. 1986).

Reentrainment of particles is not considered in the models. This phenomenon is not important at the flow rates expected. A user could add models for this, if necessary. A reference for reentrainment is the Nuclear Fuel Cycle Accident Analyses Handbook, NUREG-1320 (Ayer et al. 1988).

3.0 CODE DESCRIPTION

FPPF_2 is a small "structured" program of less than 1100 lines. The main program is primarily a driver of subroutines. Each subroutine is a module that can be easily replaced or updated.

3.1 CODE ORGANIZATION

The main driver program initially calls for the input file. Then it controls the time-marching sequence over the whole transient event, calling the CALC and INTERP subroutines where appropriate. The structure of the whole code is depicted in Figure 1.

The input file is constructed by the user. To aid in this construction the user can employ the BLDINPT2.EXE software included with the FPPF_2 code. Details of the input file construction are found in Section 4.0.

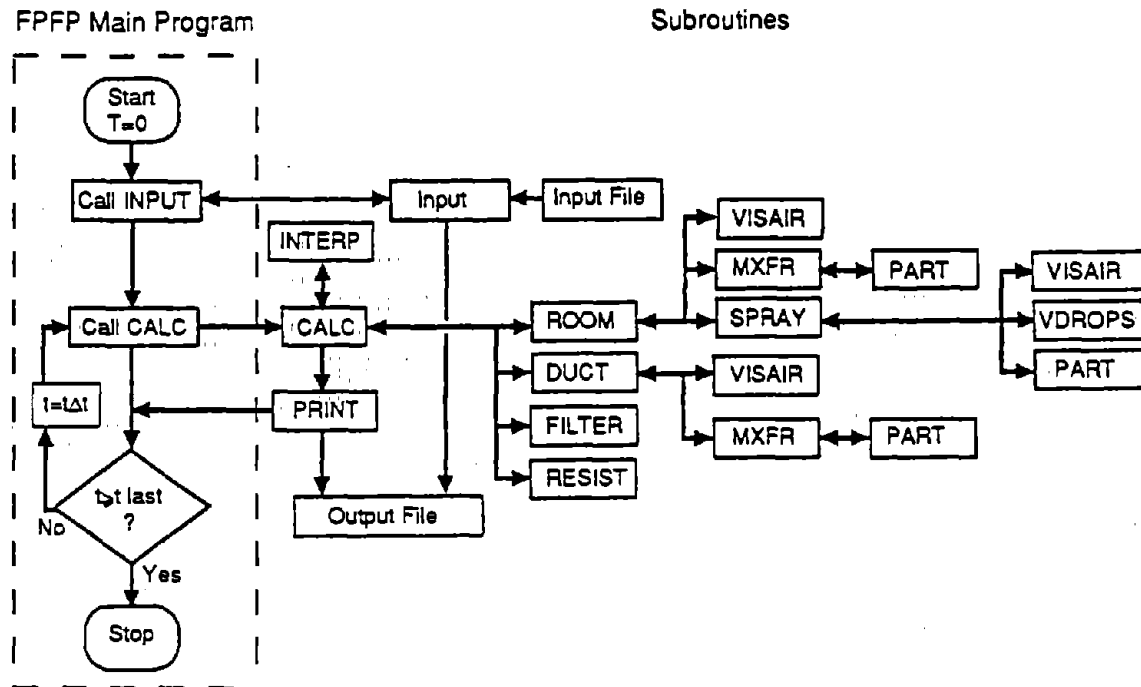


FIGURE 1. Schematic Diagram of FPPF_2 Showing Components and Information Flow

3.2 SUBROUTINES

The purpose of each of the subroutines is explained in the beginning of each subroutine. In summary, INPUT reads the input file and rewrites it in the output file; INTERP obtains (by interpolation) input data between input time values; CALC directs concentration calculations in the flow path; ROOM, DUCT, FILTER, and RESIST perform concentration calculations; and PRINT provides the output through the duration of the event.

Other subroutines that support those listed above include the following: MXFR computes mass transfer (deposition velocity) coefficients for rooms and ducts; PART calculates particle settling velocities; SPRAY computes washout coefficient for particles in spray compartments; VDROPS computes settling velocities for spray droplets; and VISAIR computes gas viscosities.

4.0 CODE OPERATION

Operating FFPF_2 requires establishing an input data file for each transient reactor accident case. Creating the input file is done by executing a code called BLDINPT2. This code prompts the user for all necessary input data and automatically creates an input file in the FFPF 2 format. The executable file, FFPF_2.EXE, which can be run on any IBM-compatible personal computer, uses the input files to calculate the desired output, and creates an output file designated by the user. The sections below describe the development of the necessary components of the input file and the output expected. Then a simple accident case demonstrates the use of the code.

4.1 BLDINPT2

Appendix A (pages A.1-A.2) defines the input and other variables. The listing of subroutine INPUT shows the order of the input variables. Using BLDINPT2 is probably the easiest way to develop an input file, even for experienced users. However, to make single variable changes from case to case, it is probably easier to change the variable in an already developed file.

4.1.1 Puff Release and Other Variables

Form 1 contains some initial naming requirements and requires defining the number of nodes, defining the puff release in space 1, if desired, and deciding whether the particle diameter as defined in the code is acceptable. The sample case in Section 4.3 will show examples of these choices.

4.1.2 Plant Variables

With Form 2, the user builds up a list of the consecutive series components of the flow path (spaces), and then establishes the dimensions of each as a rectangular parallelepiped.^(a) If the space is a duct, the angle with the horizontal is required. Additional decontamination factors (DFs) are also requested for each fission product group. Usually DFs are 1.0 except when the component is a filter.

4.1.3 Other Fission Product Sources

Form 3 allows the user to have additional fission products enter node 1 as a function of time. These additional fission products are in concentrations suggested as core fractions/ft³, but any mass unit/ft³ is satisfactory if the user makes the appropriate adjustment in interpreting the output.

(a) For example, we suggest that a round duct of length L, volume V, and radius r, where $V = \pi r^2 L$, be represented by a duct of length L, volume V, and flow cross section l^2 , such that $\pi r^2 = l^2$.

4.1.4 Gas Variables

Form 4 allows the user to develop the data file for gas flow rates and conditions. The gas temperature and pressure are used to calculate gas transport coefficients.

4.1.5 Spray Variables

Form 5 allows the addition of sprays to any room for removal of particles. The spray parameters are listed on the form. A decision is required to change the spray droplet diameters from 1 mm as coded.

4.2 OUTPUT DESCRIPTION

The output file consists of two parts. The first part of the output file is a printout of the input file, i.e., the input variable names and the input data. The second part is the output of transient accident scenario calculations.

This latter part presently consists of two sets of variables: the concentrations of fission products, in core fractions/ft³, leaving each node and the flow rates of fission products leaving the nodes. The time values at which each calculation is completed and printed are determined by an input decision.

FPP2 can be easily modified to change the printing frequency and format. Other calculations can be introduced and printed, too. These might include cumulative amounts entering a room, cumulative amounts collecting on filters, and cumulative amounts settling or plating out; a breakdown of fission products by isotope; and calculation of radioactively decayed levels of these isotopes.

4.3 SAMPLE CASE

To demonstrate the use of FPP2, a simple Sample Puff Release Case has been set up and executed. The flow path consists of five nodes and four spaces (components). Figure 2 shows the order of the components and the flow rates, which were held constant during the transient accident. At $t = 0$, the transient accident was initiated by a sudden jump in fission product concentration in Space 1 as a puff release. Please refer to the completed BLDINPT2 forms in Appendix B.1 for the Sample Puff Release Case.

Figure 2 shows each node in its generalized form. It is probably clearer to interpret the flow schematic as constant flow of 15,000 acfm from the inlet at space 1 to node 3 where 10,000 acfm splits off to some unspecified destination. The remaining 5,000 acfm continues through the remaining part of the flow path and then exits to another unspecified destination.

The number of time steps was arbitrarily chosen to equal 3 with data entry times of 0, 100, and 200 minutes. This choice separates the calculating/printing intervals by 10 minutes.

The dimensions of the rooms and duct were chosen so that their identity could not be mistaken. Any resemblance of these dimensions to those of a nuclear power plant is purely coincidental. One could imagine that space 4 could be a control room, since it is the last component in the flow path. The dimensions of the filter of 1 ft x 1 ft x 1 ft are arbitrary; the READ statement expects each component to have dimensions regardless of identity. No calculations are made with the dimensions of a filter or flow resistance.

DFs were chosen as follows: in this sample case only the filter component had DFs = 1, 20, and 2000 for noble gases, I_2 , and particles, respectively. The other components are assigned 1, 1, and 1.

The final input file is assembled in proper order in Appendix B.2. This file is read during the execution of FFPF.EXE and is reprinted with variable names in the first part of the output file found in Appendix B.2. When assembling an input file it could be useful to compare the input file with the corresponding part of the output file for this Sample Puff Release Case.

The remainder of the output is the sets of fission product concentrations and flow rates at 21 time points during the event. Three of these are reproduced in Appendix B.3; at $t = 0, 10,$ and 200 minutes. Figure 3 is a plot of the concentrations of noble gases, I_2 , and particles in space 4 over the 200-minute period. Some observations can be made in Figure 3. The pulse of the puff release builds to a maximum and then decays by dilution. The rate of decay depends primarily on the dilution time of the system. The dilution time of a single well-mixed room is equal to the volume of the room divided by the gas flow-through rate. For a series of flow path components, the dilution time is more complex. The ratios of the steady-state concentrations of I_2 and particles to noble gases with filtration alone should be 0.05 and 0.0005, respectively. Since these are 0.015 and 0.00045, respectively, some natural deposition of I_2 and particles has occurred.

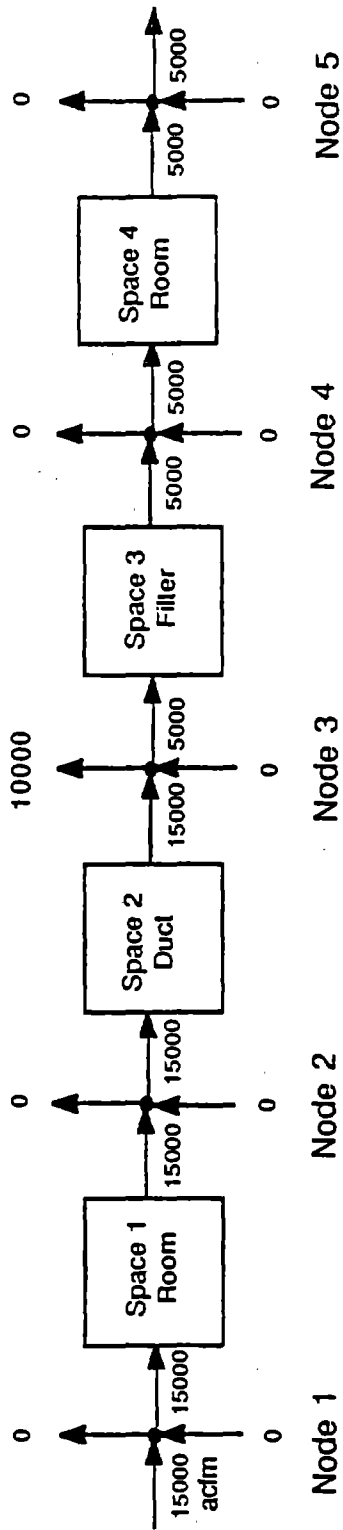


FIGURE 2. Sample Case Flow Path Showing Nodes, Components (Spaces), and Flow Rates

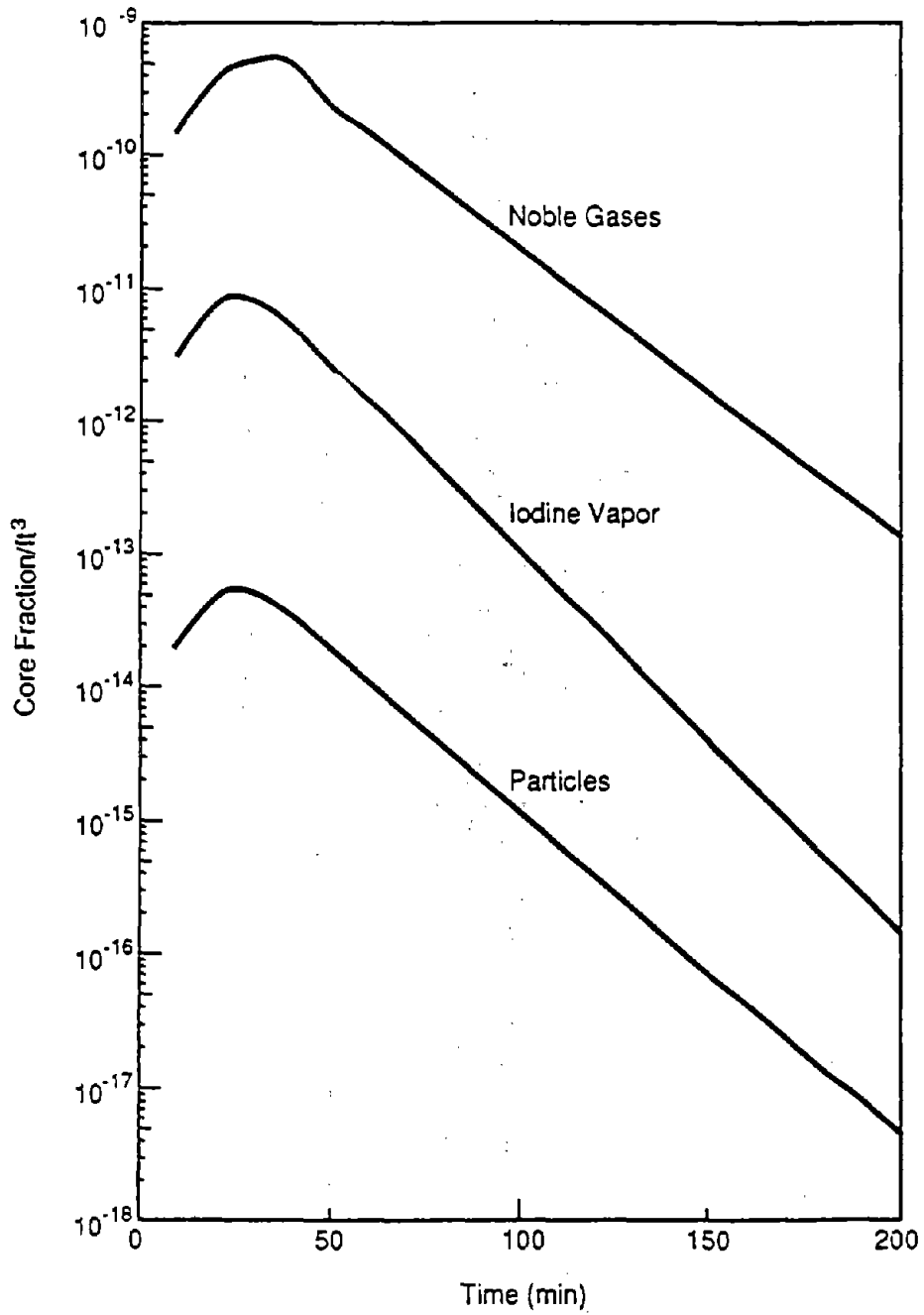


FIGURE 3. Concentration of Fission Products in Sample Case Space 4 as a Function of Time as Calculated by FFP

5.0 REFERENCES

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APPENDIX A

FPFP 2 LISTING

1. The first part of the document discusses the importance of maintaining accurate records of all transactions and activities. It emphasizes that proper record-keeping is essential for transparency and accountability, particularly in financial reporting and compliance with regulatory requirements. The text notes that incomplete or inconsistent records can lead to significant legal and financial consequences for the organization.

2. The second section addresses the challenges associated with data management in a rapidly evolving digital landscape. It highlights the need for robust security protocols to protect sensitive information from cyber threats and unauthorized access. Additionally, it discusses the importance of data integrity and the implementation of backup and recovery strategies to ensure business continuity in the event of a data loss or system outage.

3. The third part of the document focuses on the role of technology in streamlining operations and improving efficiency. It explores various digital tools and platforms that can be leveraged to automate repetitive tasks, enhance communication, and facilitate data analysis. The text suggests that investing in modern technology is crucial for staying competitive in the current market environment.

4. The final section discusses the importance of continuous learning and professional development for the workforce. It encourages organizations to provide opportunities for training and skill enhancement, as this is essential for adapting to new technologies and industry trends. The text also mentions the benefits of fostering a culture of innovation and collaboration, which can lead to increased productivity and long-term success.

COMMON/BLK2/T1,NSTEP
COMMON/BLK6/TLAST

DEFINITIONS

HEAD1=TITLE OF INPUT FILE

NDATA=2,.....,30 MAX, NO. OF TIME POINTS FOR DATA ENTRY

NODES=NO. OF NODES IN FLOW PATH, 20 MAX

NPUFF.NE.1, NO PUFF INTO SPACE 1 (ROOM) AT T=0; NPUFF=1 PLACES A PUFF
RELEASE INTO SPACE 1 WITH CONCENTRATIONS CPUFF(I), I=1,3, FOR NG, I2, AND
PARTICLES, RESPECTIVELY, IN CORE FRACTIONS/FT**3.

NPUFF = 0, NO PUFF RELEASE INTO SPACE 1 (ROOM) AT TNDATA(1); NPUFF = 1,
PUFF INTO SPACE 1 AT TNDATA(1) WITH CONCENTRATIONS CPUFF(1), CPUFF(2),
AND CPUFF(3), CORE FRACTIONS OF NG, I2, AND PARTICLES, RESPECTIVELY, IN
CORE FRACTIONS/FT**3.

DMULT=MULTIPLIER OF PARTICLE SIZE AMMD=1 MICROMETER.

TNDATA(J), J=1,NDATA, TIME VALUES AT EACH NDATA (MINUTES)

FP(I,J) = AVG FLOW RATE OF FISSION PRODUCT GROUP J FROM NODE I
INTO SPACE I. J=1=NOBLE GASES, 2=VAPOR I2, 3-7=FIVE PARTICLE
SIZES. UNITS OF FP ARE IN FRACTIONS OF CORE INVENTORY PER MINUTE.

CONC(I,J) = CONCENTRATION OF FISSION PRODUCTS AT NODE I AT TNDATA(I) FOR
FISSION PRODUCT GROUP J = 1,2, OR 3 AS ABOVE. FRACTION OF CORE INVENTORY
PER FT**3.

CNC(I,J,K) = CONCENTRATION OF FISSION PRODUCT J ENTERING NODE I AT TIME K

CNCP(I,J,K)= CONCENTRATION OF FISSION PRODUCT J LEAVING NODE I AT TIME K

FR(I,J) = FLOW RATE OF GASES (ACFM) FROM NODE J INTO SPACE J AT
TNDATA(I).

FRO(I,J) = FLOW RATE OF GASES FROM SPACE J INTO NODE J+1.

FROUT(I,J) = FLOW RATE OF GASES (ACFM) FROM NODE J OUT OF FLOW PATH
AT TNDATA(I).

FRIN(I,J) = FLOW RATE OF GASES (ACFM) INTO FLOW PATH AT NODE J AT
TNDATA(I).

PDATA(I,J) AND TDATA(I,J) ARE PSIG AND DEGREES C IN THE GAS IMMEDIATELY
DOWNSTREAM OF NODE J AT TNDATA(I).

NSPACE(J) = 1 = ROOM, = 2 = DUCT, = 3 = FILTER, = 4 = FLOW RESISTANCE (E.
G. A LEAKY DOOR). IF NPUFF=1, NSPACE(1)=1.

DT(K) = TIME STEP, MINUTES, BETWEEN TNDATA(K) AND TNDATA(K+1)

VOL(K) = HEIGHT(K)*WIDTH(K)*LENGTH(K), FT**3

AXSXN(K) = HEIGHT(K)*WIDTH(K)

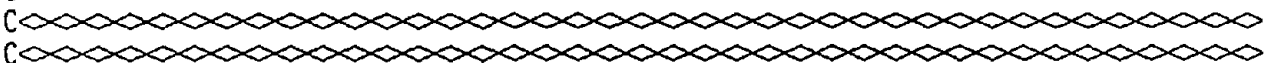
AFLOOR(K) = WIDTH(K)*LENGTH(K)

THETA(K) = ANGLE OF DUCT(K) WITH HORIZONTAL

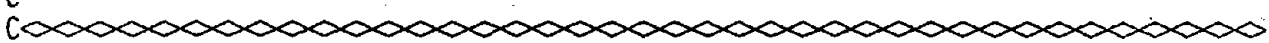
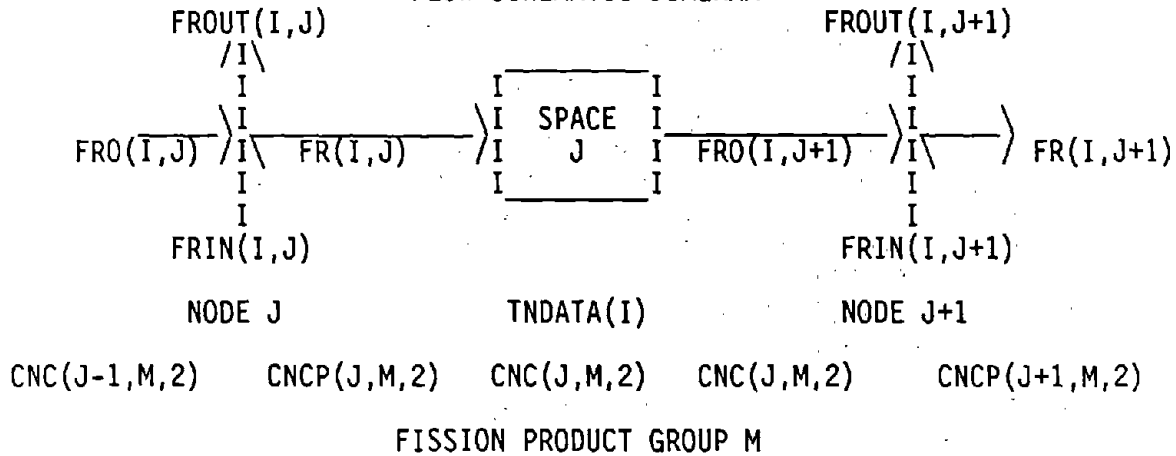
THE FOLLOWING ARE OPTIONAL SPRAY PARAMETERS:

IF ROOM J HAS A SPRAY SYSTEM THAT OPERATES BETWEEN TIMES TSON AND TSOFF,
THEN NSPRAY(J)=1, AND DSPRAY(J)=MULTIPLIER OF DROPLET MMD RELATIVE TO 1.0
MILLIMETERS, HSPRAY(J)= SPRAY HEIGHT (FT), AND VSPRAY(J)=VOL FLOW RATE

(CFM). SUBROUTINE SPRAY RETURNS WASHOUT PARAMETER LSPRAY(K) FOR EACH K
 (K=1,7) FISSION PRODUCT TYPE TO SUBROUTINE ROOM.



FLOW SCHEMATIC DIAGRAM



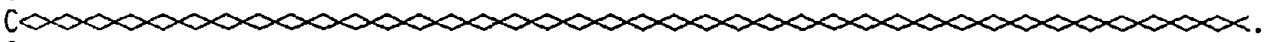
```

C      CALL INPUT
C      WRITE(6,101)
101    FORMAT(//,5X,'BEGIN PROCESSING . . .',//)
  
```

```

      TT=0.
      NSTEP=1

C      TT = TIME OF CALCULATION, MIN
  
```



```

C      PERFORM CALCULATIONS NOW
C
100   CONTINUE

      CALL CALC

C      IF(TT.GE.TLAST) GO TO 1000
C
      T1=TT
      NSTEP=NSTEP+1
      TT=TT+DTT
      GO TO 100

C
1000  CONTINUE
  
```

```
WRITE(*,'(//,A)') ' PROGRAM SUCCESSFULLY COMPLETED'  
STOP  
END
```



```

C*****
C
C
C   SUBROUTINE INPUT
C
C   THIS SUBROUTINE READS THE INPUT FILE FFPF.DAT AND PRINTS IT OUT IN
C   FFPF.OUT
C
C   CHARACTER HEAD1*80
C   CHARACTER*12  INFILE,OUTFILE,TEMP
C
C   DIMENSION DIAM(5), DIAM1(5), FRAC(5), CNC(0:19,7,2), BONC(30)
C
C   REAL LENGTH(20)
C   DIMENSION CONC(30,7), FP(20,7), FR(30,20), FROUT(30,20),
+FR0(30,20), FRIN(30,20), TNDATA(30), PDATA(30,20), TDATA(30,20),
+NSPACE(20), HEIGHT(20), WIDTH(20), DT(30), VOL(20), AXSXN(20),
+AFLOOR(20), DF1(20), DF2(20), DF3(20), FRI(20), FROUTI(20), FRINI(20),
+TDATAI(20), PDATAI(20), FROI(20), CONCI(7), CPUFF(7), NSPRAY(20)
C
C   DIMENSION DSPRAY(20), HSPRAY(20), VSPRAY(20), CNCP(20,7,2), TSON(20),
+TSOFF(20)
C   DIMENSION THETA(20)
C
C   COMMON /BLK1/TT,DT,DTT,CNC,CONC,NDATA,NODES,TNDATA,TDATA,PDATA,
+FP,FR,FRO,FROUT,FRIN,NSPACE,HEIGHT,WIDTH,LENGTH,VOL,AXSXN,AFLOOR,
+DF1,DF2,DF3,FROUTI,FRINI,FRI,FROI,PDATAI,TDATAI,CONCI,CNCP
C   COMMON/BLK6/TLAST
C   COMMON/BLK10/CPUFF,NPUFF
C   COMMON/BLK30/DIAM,VP,DIFUS,CM
C   COMMON/BLK23/TSON,TSOFF
C   COMMON/BLK24/NSPRAY
C   COMMON/BLK25/DSPRAY,HSPRAY,VSPRAY
C   COMMON/BLK90/THETA
C
C   WRITE(6,1)
1  FORMAT(' Program Title:  FFPF.'//
+ ' Developed For:  U.S. Nuclear Regulatory Commission'/
+ '                Office of Nuclear Regulatory Research'/
+ '                Division of Reactor Accident Analysis'//
+ ' Date:          June 1990'//
+ ' NRC Contact(s): C. Ferrell      Phone: (FTS) 492-3944'/
+ ' Code Developer: P. C. Owczarcki Phone: (509) 376-1701'/
+ '                (FTS) 444-1701'//
+ ' Code Documentation: '//
+ ' The program was prepared for an agency of the United States',
+ ' Government. Neither'// the United States Government nor any',
+ ' agency thereof, nor any of their'// employees, makes any',
+ ' warranty, expressed or implied, or assumes any legal'/
+ ' liability or responsibilities for any third party's use,',
+ ' or the results of such'// use, of any portion of this',

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+ ' program or represents that its use by such third/' party',
+ ' would not infringe privately owned rights. '/// )

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```

WRITE(6,2)
2  FORMAT(1X,'Hit RETURN to Continue ', $)
   READ(5,'(I1)')I

WRITE(6,600)
600 FORMAT(//,5X,'XXXXX XXXXX XXXXX XXXXX',/,
*        5X,'XX   XX XX XX   XX XX',/,
*        5X,'XXXX XXXXX XXXX  XXXXX',/,
*        5X,'XX   XX   XX   XX',/,
*        5X,'XX   XX   XX   XX',/,
*        3X,'(Fission Product Flow Path)',//)

WRITE(6,601)
601 FORMAT(3X,'ENTER THE INPUT FILENAME > ', $)
   READ(5,'(A)')INFILE
699 OPEN(UNIT=1,FILE=INFILE,STATUS='OLD',IOSTAT=IER)
   IF(IER .EQ. 6416) THEN
     WRITE(6,602)INFILE
602   FORMAT(/,5X,'* * * ',A12,' DOES NOT EXIST * * *',/)
     WRITE(6,603)
603   FORMAT(3X,'ENTER NEW FILENAME, OR <RETURN> TO STOP > ', $)
     READ(5,'(A)')TEMP
     IF(TEMP(1:3) .EQ. ' ') THEN
       WRITE(6,604)
604   FORMAT(//,5X,'<<< TERMINATING EXECUTION >>>',//)
       STOP
     ENDIF
     INFILE = TEMP
     GOTO 699
   ENDIF
   WRITE(6,605)INFILE
605   FORMAT(//,5X,'OPENED ',A12,' AS INPUT',//)
   IND = INDEX(INFILE,'.') - 1
   OUTFILE = INFILE(1:IND)//'.OUT'
   WRITE(6,606)OUTFILE,OUTFILE
606   FORMAT(5X,'OUTPUT FILE WILL BE CALLED: ',A12,/,
*        3X,'ENTER ANOTHER FILENAME, OR <RETURN> TO USE ',A12,/,
*        3X,'AS OUTPUT FILE > ', $)
   READ(5,'(A)')TEMP
   IF(TEMP(1:3) .NE. ' ') OUTFILE = TEMP
698 OPEN(UNIT=2,FILE=OUTFILE,STATUS='NEW',IOSTAT=IER)
   IF(IER .EQ. 6415) THEN
     CLOSE(2)
     WRITE(*,607)OUTFILE
607   FORMAT(/,5X,'* * * ',A12,' ALREADY EXISTS * * *',/)
     WRITE(*,608)
608   FORMAT(' ENTER A NEW FILENAME, ',
*        ' OR HIT <RETURN> TO OVERWRITE OLD FILE > ', $)
     READ(*,'(A)')TEMP
     IF(TEMP(1:3) .EQ. ' ') THEN

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```

        WRITE(*,609)OUTFILE
609      FORMAT(/,5X,A12,' WILL BE OVERWRITTEN',/)
        OPEN(UNIT=2,FILE=OUTFILE,STATUS='UNKNOWN')
        ELSE
        WRITE(*,610)TEMP
610      FORMAT(/,5X,A12,' WILL BE OPENED',/)
        OUTFILE = TEMP
        GOTO 698
        ENDIF
    ENDIF

    OPEN(UNIT=3,FILE='CRHFPPF.OUT',STATUS='UNKNOWN')
C      ABOVE LINE REQUESTED BY H. GILPIN, SAIC, 2/13/90.
C
    WRITE(2,1)
    READ(1,'(A)')HEAD1
    WRITE(2,'(A)')HEAD1
    READ(1,*)NDATA,NODES,NPUFF,DMULT
    WRITE(2,501) 'NODES=',NODES
    WRITE(2,501) 'NDATA=',NDATA
    WRITE(2,501) 'NPUFF=',NPUFF
    WRITE(2,502) 'DMULT=',DMULT
501    FORMAT(3X,A6,1X,I4)
502    FORMAT(3X,A6,1X,F9.4)

    IF(NPUFF.EQ.1)THEN
        READ(1,*)(CPUFF(I),I=1,3)
        WRITE(2,503) 'CPUFF(I)= ',(CPUFF(I),I=1,3)
    END IF
    READ(1,*)(TNDATA(I),I=1,NDATA)
    WRITE(2,503) 'TNDATA(I)=',(TNDATA(I),I=1,NDATA)
    TLAST=TNDATA(NDATA)
    DO 10 K=1,NDATA
        READ(1,*)(CONC(K,J),J=1,3)
        WRITE(2,'(3X,A4,I3)') 'K = ',K
        WRITE(2,503) 'CONC(K,J)=',(CONC(K,J),J=1,3)
10    CONTINUE
503    FORMAT(3X,A10,5(3X,1PE10.4),/,13X,5(3X,1PE10.4),/,
*        13X,5(3X,1PE10.4),/,13X,5(3X,1PE10.4))

    DO 20 K=1,NODES-1
        READ(1,*)NSPACE(K),HEIGHT(K),WIDTH(K),LENGTH(K),DF1(K),DF2(K),
+        DF3(K)
        WRITE(2,504)K,NSPACE(K),HEIGHT(K),WIDTH(K),LENGTH(K),
*        DF1(K),DF2(K),DF3(K)
504    FORMAT(/,3X,'SPACE # K=',I3,3X,'NSPACE(K)=',I3,/,
*        5X,'HEIGHT(K)=',F9.3,3X,'WIDTH(K)=',F9.3,
*        5X,'LENGTH(K)=',F9.3,/,
*        5X,'DF1(K)= ',1PE10.4,4X,'DF2(K)= ',1PE10.4,
*        5X,'DF3(K)= ',1PE10.4)

    THETA(K) = 0.0

```

```

      IF(NSPACE(K) .EQ. 2) THEN
        READ(1,*)THETA(K)
        WRITE(2,505)K,THETA(K)
505      FORMAT(5X,'SPACE #',I2,' IS A DUCT, AND HAS AN ANGLE WITH',
      *          ' THE HORIZONTAL = ',F6.2,' DEGREES')
        THETA(K) = THETA(K) * ( 3.141592654 / 180.0 )
      C      CONVERT THETA FROM DEGREES TO RADIANS
        ENDIF
20    CONTINUE
      WRITE(2,*)
      DO 30 J=1,NODES
        WRITE(2,506)J,NDATA
506      FORMAT(3X,'NODE ',I2,' NDATA = 1... ',I2)
507      FORMAT(3X,A11,5(3X,F10.3),/,14X,5(3X,F10.3),/,
      *          14X,5(3X,F10.3),/,14X,5(3X,F10.3),/,
      *          14X,5(3X,F10.3),/,14X,5(3X,F10.3))
508      FORMAT(3X,A33)
        READ(1,*)(FR(K,J),K=1,NDATA)
        WRITE(2,507) 'FR(K,J)= ',(FR(K,J),K=1,NDATA)
        READ(1,*)(FRO(K,J),K=1,NDATA)
        WRITE(2,507) 'FRO(K,J)= ',(FRO(K,J),K=1,NDATA)
        READ(1,*)(FROUT(K,J),K=1,NDATA)
        WRITE(2,507) 'FROUT(K,J)= ',(FROUT(K,J),K=1,NDATA)
        READ(1,*)(FRIN(K,J),K=1,NDATA)
        WRITE(2,507) 'FRIN(K,J)= ',(FRIN(K,J),K=1,NDATA)
        READ(1,*)(PDATA(K,J),K=1,NDATA)
        WRITE(2,507) 'PDATA(K,J)= ',(PDATA(K,J),K=1,NDATA)
        READ(1,*)(TDATA(K,J),K=1,NDATA)
        WRITE(2,507) 'TDATA(K,J)= ',(TDATA(K,J),K=1,NDATA)
30    CONTINUE

      DO 40 K=1,NODES-1
        IF(NSPACE(K) .LE.2) AXSXN(K)=HEIGHT(K)*WIDTH(K)
        IF(NSPACE(K) .LE.2) AFLOOR(K)=WIDTH(K)*LENGTH(K)
        IF(NSPACE(K) .LE.2) VOL(K)=AXSXN(K)*LENGTH(K)
        IF(NSPACE(K) .EQ.1) READ(1,*) NSPRAY(K)
        IF(NSPRAY(K) .EQ.1) THEN
          WRITE(2,*) 'SPACE # ',K,' HAS A SPRAY SYSTEM WHERE:'
          READ(1,*) DSPRAY(K),HSPRAY(K),VSPRAY(K),TSON(K),TSOFF(K)
          WRITE(2,*) ' DSPRAY= ',DSPRAY(K),' DROPLET DIAMETER MULTIPLIER'
          WRITE(2,*) ' HSPRAY= ',HSPRAY(K),' SPRAY HEIGHT, FT'
          WRITE(2,*) ' VSPRAY= ',VSPRAY(K),' VOL. SPRAY RATE, GPM'
          WRITE(2,*) ' TSON= ',TSON(K),' TIME SPRAYS GO ON, MIN'
          WRITE(2,*) ' TSOFF= ',TSOFF(K),' TIME SPRAYS GO OFF, MIN'
        ENDIF
40    CONTINUE
      C
      C      THE NEXT DO LOOPS ASSIGN PARTICLES TO FIVE BUCKETS REPRESENTING A
      C      LOGNORMAL DISTRIBUTION AROUND ONE MICRON AMMD WITH GEOMETRIC STANDARD
      C      DEVIATION OF 2.0.
      C

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```
DATA DIAM1/.158489,.398107,1.,2.51189,6.30957/
DATA FRAC/.0156896,.219259,.530103,.219259,.0156896/
DO 50 J=1,NDATA
  BONC(J)=CONC(J,3)
  DO 50 K=3,7
    CONC(J,K)=FRAC(K-2)*BONC(J)
    DIAM(K-2)=DIAM1(K-2)*DMULT
50 CONTINUE

  IF(NPUFF.EQ.1)THEN
    PUFFC=CPUFF(3)
    DO 60 K=3,7
      CPUFF(K)=PUFFC*FRAC(K-2)
60 CONTINUE
  ENDIF

800 FORMAT(1X,A,T15,7(2X,E11.5))
RETURN
END
```

```

C*****
C
C
C      SUBROUTINE INTERP
C
C      THIS SUBROUTINE PERFORMS LINEAR INTERPOLATIONS FOR TT BETWEEN TNDATA(K)
C      AND TNDATA(K+1).
C
C      REAL LENGTH(20)
C      DIMENSION CONC(30,7),FP(20,7),FR(30,20),FROUT(30,20),
C      +FRO(30,20),FRIN(30,20),TNDATA(30),PDATA(30,20),TDATA(30,20),
C      +NSPACE(20),HEIGHT(20),WIDTH(20),DT(30),VOL(20),AXSXN(20),
C      +AFLOOR(20),DF1(20),DF2(20),DF3(20),FRI(20),FROUTI(20),FRINI(20),
C      +TDATAI(20),PDATAI(20),FROI(20),CONCI(7)
C
C      DIMENSION CNC(0:19,7,2),CNCP(20,7,2)
C      COMMON /BLK1/TT,DT,DTT,CNC,CONC,NDATA,NODES,TNDATA,TDATA,PDATA,
C      +FP,FR,FRO,FROUT,FRIN,NSPACE,HEIGHT,WIDTH,LENGTH,VOL,AXSXN,AFLOOR,
C      +DF1,DF2,DF3,FROUTI,FRINI,FRI,FROI,PDATAI,TDATAI,CONCI,CNCP
C
C      DO 10 J=1,NDATA-1
C      IF(TT.GE.TNDATA(J).AND.TT.LE.TNDATA(J+1)) INTER=J
10 CONTINUE
C
C      DEL=TNDATA(INTER+1)-TNDATA(INTER)
C      DELT=TT-TNDATA(INTER)
C      DTT=DEL/10.
C      DO 20 K=1,NODES
C      DFR=FR(INTER+1,K)-FR(INTER,K)
C      FRI(K)=FR(INTER,K)+DFR*DELT/DEL
C      DFRO=FRO(INTER+1,K)-FRO(INTER,K)
C      FROI(K)=FRO(INTER,K)+DFRO*DELT/DEL
C      DFROUT=FROUT(INTER+1,K)-FROUT(INTER,K)
C      FROUTI(K)=FROUT(INTER,K)+DFROUT*DELT/DEL
C      DFRIN=FRIN(INTER+1,K)-FRIN(INTER,K)
C      FRINI(K)=FRIN(INTER,K)+DFRIN*DELT/DEL
C      DTDATA=TDATA(INTER+1,K)-TDATA(INTER,K)
C      TDATAI(K)=TDATA(INTER,K)+DTDATA*DELT/DEL
C      DPDATA=PDATA(INTER+1,K)-PDATA(INTER,K)
C      PDATAI(K)=PDATA(INTER,K)+DPDATA*DELT/DEL
20 CONTINUE
C
C      DO 30 K=1,7
C      IF(TT.EQ.0.) THEN
C      CONCI(K)=CONC(1,K)
C      CNC(0,K,1)=CONCI(K)
C      CNCP(1,K,1)=CNC(0,K,1)*FRO(1,1)/(FROUT(1,1)+FR(1,1))
C      CNC(0,K,2)=CNC(0,K,1)
C      CNCP(1,K,2)=CNCP(1,K,1)
C      FP(1,K)=CNCP(1,K,2)*FRI(1)
C      END IF

```

```

IF(TT.GT.0.)THEN
  DCONC=CONC(INTER+1,K)-CONC(INTER,K)
  CONCP=CONCI(K)
  CONCI(K)=CONC(INTER,K)+DCONC*DELT/DEL
  CNC(0,K,1)=(CONCI(K)+CONCP)/2.
  CNCP(1,K,1)=CNC(0,K,1)*FROI(1)/(FROUTI(1)+FRI(1))
  CNC(0,K,2)=CONCI(K)
  CNCP(1,K,2)=CNC(0,K,2)*FROI(1)/(FROUTI(1)+FRI(1))
  END IF
30 CONTINUE
C
  RETURN
  END

C*****
C
C
C
SUBROUTINE CALC

C
C
C
C
THIS SUBROUTINE DRIVES THE CALCULATION PROCESSES FOR THE TRANSPORT
AND DEPOSITION OF FISSION PRODUCTS

C
C
REAL LENGTH(20)
DIMENSION CONC(30,7),FP(20,7),FR(30,20),FROUT(30,20),
+FR(30,20),FRIN(30,20),TNDATA(30),PDATA(30,20),TDATA(30,20),
+NSPACE(20),HEIGHT(20),WIDTH(20),DT(30),VOL(20),AXSXN(20),
+AFLOOR(20),DF1(20),DF2(20),DF3(20),FRI(20),FROUTI(20),FRINI(20),
+TDATAI(20),PDATAI(20),FROI(20),CONCI(7),CPUFF(7),NSPRAY(20)

DIMENSION CNC(0:19,7,2),CNCP(20,7,2),cncr(20,7,2)

COMMON /BLK1/TT,DT,DTT,CNC,CONC,NDATA,NODES,TNDATA,TDATA,PDATA,
+FP,FR,FRO,FROUT,FRIN,NSPACE,HEIGHT,WIDTH,LENGTH,VOL,AXSXN,AFLOOR,
+DF1,DF2,DF3,FROUTI,FRINI,FRI,FROI,PDATAI,TDATAI,CONCI,CNCP
COMMON/BLK2/T1,NSTEP
COMMON/BLK3/ISPACE
COMMON/BLK10/CPUFF,NPUFF
common/blk60/cncr

C
CALL INTERP

DO 10 I=1,NODES-1
  ISPACE=I
  IF(TT.EQ.0.) GO TO 9
  IF(NSPACE(I).EQ.1)CALL ROOM
  IF(NSPACE(I).EQ.2)CALL DUCT
  IF(NSPACE(I).EQ.3)CALL FILTER
  IF(NSPACE(I).EQ.4)CALL RESIST

```

```

9 CONTINUE
  IF(TT.EQ.0.)THEN
    DO 8 M=1,7
      CNC(ISPACE,M,2)=0.
      IF(ISPACE.EQ.1.AND.NPUFF.EQ.1)CNC(1,M,2)=CPUFF(M)
8 CONTINUE
    END IF
C
    DO 11 M=1,7
      CAVGO=(CNC(I,M,2)+CNC(I,M,1))/2.
      IF(TT.EQ.0.)CAVGO=CNC(I,M,1)
      SPLIT=FROI(I+1)/(FROUTI(I+1)+FRI(I+1))
      CNCP(I+1,M,2)=CAVGO*SPLIT
      cncr(i+1,m,2)=cnc(i+1,m,2)*split
      FP(I+1,M)=CNCP(I+1,M,2)*FRI(I+1)
11 CONTINUE
10 CONTINUE
C
    CALL PRINT
C
    RESET CNC & CNCP FOR NEXT TIME STEP.  ADD NON-ZERO DELC TO AVOID CRASH.
    DELC=1.E-20
    DO 20 M=0,NODES-1
      DO 20 N=1,7
        CNC(M,N,1)=CNC(M,N,2)+DELC
20 CONTINUE
      DO 21 M=1, NODES
        DO 21 N=1,7
          CNCP(M,N,1)=CNCP(M,N,2)
21 CONTINUE
C
C
    RETURN
    END

```



```

C*****
C
C
C   SUBROUTINE ROOM
C
C   THIS SUBROUTINE CALCULATES CNC(ISPACE,J,2) WITHIN A ROOM DESIGNATED AS
C   ISPACE IN SUBROUTINE CALC FOR FISSION PRODUCT GROUP J AT TIME = TT.
C   ALSO THE FISSION PRODUCT FLOW RATES FP(ISPACE,J) ARE ALSO CALCULATED.
C
C   REAL LENGTH(20),KP(7),KMXFR(7),LSPRAY(7)
C   DIMENSION CONC(30,7),FP(20,7),FR(30,20),FROUT(30,20),
C   +FRO(30,20),FRIN(30,20),TNDATA(30),PDATA(30,20),TDATA(30,20),
C   +NSPACE(20),HEIGHT(20),WIDTH(20),DT(30),VOL(20),AXSXN(20),
C   +AFLOOR(20),DF1(20),DF2(20),DF3(20),FRI(20),FROUTI(20),FRINI(20),
C   +TDATAI(20),PDATAI(20),FROI(20),CONCI(7),CPUFF(7),NSPRAY(20)
C
C   DIMENSION CNC(0:19,7,2),CNCP(20,7,2)
C   DIMENSION DSPRAY(20),HSPRAY(20),VSPRAY(20),TSON(20),TSOFF(20)
C
C   COMMON /BLK1/TT,DT,DTT,CNC,CONC,NDATA,NODES,TNDATA,TDATA,PDATA,
C   +FP,FR,FRO,FROUT,FRIN,NSPACE,HEIGHT,WIDTH,LENGTH,VOL,AXSXN,AFLOOR,
C   +DF1,DF2,DF3,FROUTI,FRINI,FRI,FROI,PDATAI,TDATAI,CONCI,CNCP
C
C   COMMON/BLK2/T1,NSTEP
C   COMMON/BLK3/ISPACE
C   COMMON/BLK5/KMXFR,KP,JMXFR
C   COMMON/BLK15/DIAM
C   COMMON/BLK23/TSON,TSOFF
C   COMMON/BLK24/NSPRAY
C   COMMON/BLK25/DSPRAY,HSPRAY,VSPRAY
C   COMMON/BLK40/TB,VIS,PSPACE
C   COMMON/BLK50/LSPRAY
C
C
C
C   TB=TDATAI(ISPACE)+273.16
C   PSPACE=(PDATAI(ISPACE)+14.7)/14.7
C   CALL VISAIR
C
C   DT1=TT-T1
C
C   IF(TT.EQ.0.)GO TO 21
C   DO 20 K=1,7
C   JMXFR=K
C   FP(ISPACE,K)=FRI(ISPACE)*CNCP(ISPACE,K,2)
C   A1=FP(ISPACE,K)
C   CALL MXFR
C   B1=FROI(ISPACE+1)+KMXFR(K)
C   IF(NSPRAY(ISPACE).NE.1) GO TO 40
C   IF(TT.LT.TSON(ISPACE).OR.TT.GT.TSOFF(ISPACE)) GO TO 40
C   CALL SPRAY
C   B1=B1+LSPRAY(K)*VOL(ISPACE)

```

```

40 CONTINUE
   C1=CNC(ISPACE,K,1)
C
   IF(B1.GT.0.)THEN
     C2=(A1-(A1-B1*C1)*EXP(-B1*DT1/VOL(ISPACE)))/B1
     CNC(ISPACE,K,2)=C2
     END IF
   IF(B1.LE.0.) CNC(ISPACE,K,2)=C1*(1.+A1*DT1)
20 CONTINUE
C
   WRITE(2,*) ' KMXFR= ',(KMXFR(K),K=1,7)
21 CONTINUE

RETURN
END

```

```

C*****
C
C
C      SUBROUTINE DUCT
C
C      THIS SUBROUTINE CALCULATES CNC(ISPACE,J,2) EXITING A DUCT DESIGNATED AS
C      ISPACE IN SUBROUTINE CALC FOR FISSION PRODUCT GROUP J AT TIME = TT
C
C      REAL LENGTH(20), KP(7), KMXFR(7)
C      DIMENSION CONC(30,7), FP(20,7), FR(30,20), FROUT(30,20),
C      +FRO(30,20), FRIN(30,20), TNDATA(30), PDATA(30,20), TDATA(30,20),
C      +NSPACE(20), HEIGHT(20), WIDTH(20), DT(30), VOL(20), AXSXN(20),
C      +AFLOOR(20), DF1(20), DF2(20), DF3(20), FRI(20), FROUTI(20), FRINI(20),
C      +TDATAI(20), PDATAI(20), FROI(20), CONCI(7), CNCP(20,7,2)
C
C      DIMENSION VEL(300,20), DZ(300,20), CO(300,20,7), ALPH(7), CNC(0:19,7,
C      +2)
C
C      COMMON /BLK1/TT,DT,DTT,CNC,CONC,NDATA,NODES,TNDATA,TDATA,PDATA,
C      +FP,FR,FRO,FROUT,FRIN,NSPACE,HEIGHT,WIDTH,LENGTH,VOL,AXSXN,AFLOOR,
C      +DF1,DF2,DF3,FROUTI,FRINI,FRI,FROI,PDATAI,TDATAI,CONCI,CNCP
C      COMMON/BLK2/T1,NSTEP
C      COMMON/BLK3/ISPACE
C      COMMON/BLK5/KMXFR,KP,JMXFR
C      COMMON/BLK40/TB,VIS,PSPACE
C
C      TB=TDATAI(ISPACE)+273.16
C      PSPACE=(PDATAI(ISPACE)+14.7)/14.7
C      CALL VISAIR
C
C      VEL(NSTEP,ISPACE)=FRI(ISPACE)/AXSXN(ISPACE)
C      DZ(NSTEP,ISPACE)=VEL(NSTEP,ISPACE)*DTT
C
C      DO 1 JFP=1,7
C      CO(NSTEP,ISPACE,JFP)=CNCP(ISPACE,JFP,2)
C 1 CONTINUE
C
C      SUMZ=0.
C      DO 10 J=NSTEP,1,-1
C      SUMZ=SUMZ+DZ(J,ISPACE)
C      JUMP=J
C      IF(SUMZ.GE.LENGTH(ISPACE)) GO TO 20
C 10 CONTINUE
C      IF(SUMZ.LT.LENGTH(ISPACE)) GO TO 30
C 20 CONTINUE
C      DTP=SUMZ-LENGTH(ISPACE)
C
C      DO 40 JFP=1,7
C      JMXFR=JFP
C      CALL MXFR
C      CALL MXFR PRODUCES A MASS TRANSFER COEFFICIENT,AKP, IN 1/MIN
C
C

```

```
ALPH(JFP)=DTP*KP(JFP)/VEL(JUMP, ISPACE)
DO 40 NR=NSTEP, JUMP+1, -1
CALL MXFR
ALPH(JFP)=ALPH(JFP)+DZ(NR, ISPACE)*KP(JFP)/VEL(NR, ISPACE)
40 CONTINUE
C
DO 50 JFP=1,7
EX=EXP(-ALPH(JFP))
CNC(ISPACE, JFP, 2)=CO(JUMP, ISPACE, JFP)*EX
50 CONTINUE
GO TO 70
30 CONTINUE
DO 60 JFP=1,7
CNC(ISPACE, JFP, 2)=0.
60 CONTINUE
70 CONTINUE
C
RETURN
END
```

```
C*****  
C  
C  
C  
C  
C  
C  
C
```

SUBROUTINE FILTER

THIS SUBROUTINE COMPUTES FISSION PRODUCT CONCENTRATIONS AFTER PASSAGE OF GAS THROUGH A SPACE "I" DESIGNATED AS A FILTER IN SUBROUTINE CALC BY THE CHOICE OF NSPACE(I)=3 IN THE INPUT DATA FILE FFP.DAT.

```
REAL LENGTH(20)  
DIMENSION CONC(30,7),FP(20,7),FR(30,20),FROUT(30,20),  
+FRO(30,20),FRIN(30,20),TNDATA(30),PDATA(30,20),TDATA(30,20),  
+NSPACE(20),HEIGHT(20),WIDTH(20),DT(30),VOL(20),AXSXN(20),  
+AFLOOR(20),DF1(20),DF2(20),DF3(20),FRI(20),FROUTI(20),FRINI(20),  
+TDATAI(20),PDATAI(20),FROI(20),CONCI(7)
```

```
DIMENSION CNC(0:19,7,2),CNCP(20,7,2)
```

```
COMMON /BLK1/TT,DT,DTT,CNC,CONC,NDATA,NODES,TNDATA,TDATA,PDATA,  
+FP,FR,FRO,FROUT,FRIN,NSPACE,HEIGHT,WIDTH,LENGTH,VOL,AXSXN,AFLOOR,  
+DF1,DF2,DF3,FROUTI,FRINI,FRI,FROI,PDATAI,TDATAI,CONCI,CNCP  
COMMON/BLK3/ISPACE
```

```
CNC(ISPACE,1,2)=CNCP(ISPACE,1,2)/DF1(ISPACE)
```

```
CNC(ISPACE,2,2)=CNCP(ISPACE,2,2)/DF2(ISPACE)
```

```
DO 10 JFP=3,7  
CNC(ISPACE,JFP,2)=CNCP(ISPACE,JFP,2)/DF3(ISPACE)
```

```
10 CONTINUE
```

```
RETURN  
END
```

```
C*****
C
C
C SUBROUTINE RESIST
C
C THIS SUBROUTINE COMPUTES FISSION PRODUCT CONCENTRATIONS AFTER PASSAGE
C OF GAS THROUGH A SPACE "I" DESIGNATED AS A FLOW RESISTANCE IN SUBROUTINE
C CALC FOR THE CHOICE OF NSPACE(I)=4 IN THE INPUT DATA FILE FPPF.DAT.
C
```

```
REAL LENGTH(20)
DIMENSION CONC(30,7),FP(20,7),FR(30,20),FROUT(30,20),
+FR0(30,20),FRIN(30,20),TNDATA(30),PDATA(30,20),TDATA(30,20),
+NSPACE(20),HEIGHT(20),WIDTH(20),DT(30),VOL(20),AXSXN(20),
+AFLOOR(20),DF1(20),DF2(20),DF3(20),FRI(20),FROUTI(20),FRINI(20),
+TDATAI(20),PDATAI(20),FROI(20),CONCI(7)
```

```
DIMENSION CNC(0:19,7,2),CNCP(20,7,2)
```

```
COMMON /BLK1/TT,DT,DTT,CNC,CONC,NDATA,NODES,TNDATA,TDATA,PDATA,
+FP,FR,FRO,FROUT,FRIN,NSPACE,HEIGHT,WIDTH,LENGTH,VOL,AXSXN,AFLOOR,
+DF1,DF2,DF3,FROUTI,FRINI,FRI,FROI,PDATAI,TDATAI,CONCI,CNCP
COMMON/BLK3/ISPACE
```

```
CNC(ISPACE,1,2)=CNCP(ISPACE,1,2)
```

```
CNC(ISPACE,2,2)=CNCP(ISPACE,2,2)
```

```
DO 10 JFP=3,7
CNC(ISPACE,JFP,2)=CNCP(ISPACE,JFP,2)
10 CONTINUE
```

```
RETURN
END
```

```

C*****
C
C
C      SUBROUTINE MXFR
C
C      THIS SUBROUTINE ESTIMATES MASS TRANSFER COEFFICIENTS FOR 12 VAPOR
C      DEPOSITION ON SURFACES AND PARTICLE SETTLING ON FLOORS.
C
C      REAL LENGTH(20), KP(7), KMXFR(7)
C      DIMENSION CONC(30,7), FP(20,7), FR(30,20), FROUT(30,20),
C      +FRO(30,20), FRIN(30,20), TNDATA(30), PDATA(30,20), TDATA(30,20),
C      +NSPACE(20), HEIGHT(20), WIDTH(20), DT(30), VOL(20), AXSXN(20),
C      +AFLOOR(20), DF1(20), DF2(20), DF3(20), FRI(20), FROUTI(20), FRINI(20),
C      +TDATAI(20), PDATAI(20), FROI(20), CONCI(7)
C      DIMENSION CNC(0:19,7,2), DIAM(5), CNCP(20,7,2)
C      DIMENSION THETA(20)
C      COMMON /BLK1/TT,DT,DTT,CNC,CONC,NDATA,NODES,TNDATA,TDATA,PDATA,
C      +FP,FR,FRO,FROUT,FRIN,NSPACE,HEIGHT,WIDTH,LENGTH,VOL,AXSXN,AFLOOR,
C      +DF1,DF2,DF3,FROUTI,FRINI,FRI,FROI,PDATAI,TDATAI,CONCI,CNCP
C
C      COMMON/BLK3/ISPACE
C
C      COMMON/BLK5/KMXFR,KP,JMXFR
C      COMMON/BLK40/TB,VIS,PSPACE
C      COMMON/BLK30/DIAM,VP,DIFUS,CM
C      COMMON/BLK90/THETA
C
C      DEPOSITION VELOCITIES, VS, FT/MIN
C
C      THE VALUES OF VS BELOW ARE FOR FIXED CONDITIONS AND FIXED PARTICLE SIZES
C      IF(JMXFR.EQ.1)VS=0.
C      IF(JMXFR.EQ.2)VS=0.1732
C
C      IF(JMXFR.GE.3)CALL PART
C      IF(JMXFR.GE.3)VS=VP*1.9685 * COS(THETA(ISPACE))
C
C      IF(NSPACE(ISPACE).EQ.1) GO TO 10
C      F1=(WIDTH(ISPACE)+HEIGHT(ISPACE))/WIDTH(ISPACE)/HEIGHT(ISPACE)
C      IF(JMXFR.LE.2)KP(JMXFR)=VS*2.*F1
C      IF(JMXFR.GE.3)KP(JMXFR)=VS/HEIGHT(ISPACE)
C
C 10 CONTINUE
C
C      AWALL=HEIGHT(ISPACE)*LENGTH(ISPACE)
C      ATOTAL=2.*(AXSXN(ISPACE)+AFLOOR(ISPACE)+AWALL)
C      IF(JMXFR.LE.2)KMXFR(JMXFR)=VS*ATOTAL
C      IF(JMXFR.GE.3)KMXFR(JMXFR)=VS*AFLOOR(ISPACE)
C
C      RETURN
C      END

```

```

C*****
C
C
C   SUBROUTINE PRINT
C
C   THIS SUBROUTINE PRINTS DESIRED CALCULATED OUTPUT TO FILE FFPF.OUT
C
C   REAL LENGTH(20)
C   DIMENSION CONC(30,7),FP(20,7),FR(30,20),FROUT(30,20),
C   +FRO(30,20),FRIN(30,20),TNDATA(30),PDATA(30,20),TDATA(30,20),
C   +NSPACE(20),HEIGHT(20),WIDTH(20),DT(30),VOL(20),AXSXN(20),
C   +AFLOOR(20),DF1(20),DF2(20),DF3(20),FRI(20),FROUTI(20),FRINI(20),
C   +TDATAI(20),PDATAI(20),FROI(20),CONCI(7),CPRNTN(20,3)
C
C   DIMENSION CPRINT(20,3),FPRINT(20,3),CNC(0:19,7,2),CNCP(20,7,2),
C   +cncr(20,7,2),cprnt(20,3)
C
C   COMMON /BLK1/TT,DT,DTT,CNC,CONC,NDATA,NODES,TNDATA,TDATA,PDATA,
C   +FP,FR,FRO,FROUT,FRIN,NSPACE,HEIGHT,WIDTH,LENGTH,VOL,AXSXN,AFLOOR,
C   +DF1,DF2,DF3,FROUTI,FRINI,FRI,FROI,PDATAI,TDATAI,CONCI,CNCP
C
C   common/blk60/cncr
C
C   DO 10 I=1,NODES
C   CPRINT(I,3)=CNC(I-1,3,2)+CNC(I-1,4,2)+CNC(I-1,5,2)+
C   +CNC(I-1,6,2)+CNC(I-1,7,2)
C   CPRNTN(I,3)=CNCP(I,3,2)+CNCP(I,4,2)+CNCP(I,5,2)+CNCP(I,6,2)+
C   +CNCP(I,7,2)
C   cprnt(i,3)=cncr(i,3,2)+cncr(i,4,2)+cncr(i,5,2)+cncr(i,6,2)+
C   +cncr(i,7,2)
C   DO 10 J=1,2
C   CPRINT(I,J)=CNC(I-1,J,2)
C   CPRNTN(I,J)=CNCP(I,J,2)
C   cprnt(i,j)=cncr(i,j,2)
10 CONTINUE
C   DO 20 I=1,NODES
C   FPRINT(I,1)=FP(I,1)
C   FPRINT(I,2)=FP(I,2)
C   FPRINT(I,3)=FP(I,3)+FP(I,4)+FP(I,5)+FP(I,6)+FP(I,7)
20 CONTINUE
C
299 FORMAT(5(5X,1PE10.4),/,5(5X,1PE10.4),/,
*       5(5X,1PE10.4),/,5(5X,1PE10.4))
C
C   WRITE(2,200)TT
200 FORMAT(/,/,/,/,/,1X,T20,'CALCULATED OUTPUT AT ',F8.2,' MINUTES'
+/,/,/,/)
C   WRITE(2,201)
201 FORMAT(1X,'CONCENTRATIONS ENTERING NODES, CORE FRACTIONS/FT**3',/,
+/,1X,'NOBLE GASES',/)
C   WRITE(2,299)(CPRINT(I,1),I=1,NODES)
C   WRITE(2,202)

```



```

202 FORMAT(/,/,1X,' IODINE, I2',/)
WRITE(2,299)(CPRINT(I,2),I=1,NODES)
WRITE(2,203)
203 FORMAT(/,/,1X,' PARTICLES',/)
WRITE(2,299)(CPRINT(I,3),I=1,NODES)
WRITE(2,205)
205 FORMAT(/,/,/,1X,' CONCENTRATIONS LEAVING NODES, CORE FRACTIONS/
+FT**3',/,/,1X,' NOBLE GASES',/)
WRITE(2,299)(CPRINT(I,1),I=1,NODES)
WRITE(2,206)
206 FORMAT(/,/,1X,' IODINE, I2',/)
WRITE(2,299)(CPRINT(I,2),I=1,NODES)
WRITE(2,207)
207 FORMAT(/,/,1X,' PARTICLES',/)
WRITE(2,299)(CPRINT(I,3),I=1,NODES)
WRITE(2,204)
204 FORMAT(/,/,/,1X,' AVG RATES OF FISSION PRODUCTS LEAVING NODES, CORE
+ FRACTIONS/MIN',/,/,1X,' NOBLE GASES',/)
WRITE(2,299)(FPRINT(I,1),I=1,NODES)
WRITE(2,202)
WRITE(2,299)(FPRINT(I,2),I=1,NODES)
WRITE(2,203)
WRITE(2,299)(FPRINT(I,3),I=1,NODES)

```

C
C

```

WRITE(3,*)(CPRINT(NODES,I),I=1,3),TT
ABOVE LINE REQUESTED BY H. GILPIN, SAIC, 2/13/90

```

```

RETURN
END

```

C*****

C

SUBROUTINE VISAIR

C

C

C

THIS SUBROUTINE COMPUTES THE VISCOSITY OF AIR AT TEMPERATURE TB, DEG K

C

COMMON/BLK40/TB,VIS,PSPACE

SIGAIR=3.617

EPSAIR=97.

OMAIR=0.765+0.82*EPSAIR/TB

VIS=2.6693E-05*SQRT(29./TB)/((SIGAIR**2.)*OMAIR)

C

C

VIS IN POISES. SEE REFERENCE BELOW:

C

BIRD, R.B., W.E. STEWART, AND E.N. LIGHTFOOT. 1960.

C

TRANSPORT PHENOMENA, JOHN WILEY & SONS, NEW YORK.

C

RETURN

END

C*****

SUBROUTINE VDROPS

C THIS SUBROUTINE CALCULATES THE VELOCITY OF FALLING WATER DROPS AS A
C FUNCTION OF DROP SIZE AND TEMPERATURE.

COMMON/BLK20/DROPDM, VDROP
COMMON/BLK40/TB, VIS, PSPACE
G=980.

RHOGAS=29.*PSPACE/82.06/TB
FDRE=1.3333*RHOGAS*G*DROPDM**3./VIS**2.
IF(FDRE.LT.10700.)RE=(FDRE/15.71)**0.7027
IF(FDRE.GE.10700.)RE=(FDRE/6.477)**0.6215

VDROP=RE*VIS/RHOGAS/DROPDM

C VDROP IN CM/S. SEE REFERENCE BELOW:
C U.S. NRC. 1975. REACTOR SAFETY STUDY, WASH-1400 (NUREG-75/014),
C APPENDIX VII, PP. VII-245. U.S. NUCLEAR REGULATORY COMMISSION,
C WASHINGTON D.C.

RETURN
END

C*****

SUBROUTINE PART

C THIS SUBROUTINE CALCULATES THE SETTLING VELOCITY, VP, DIFFUSIVITY, DIFUS,
C CM, AND CUNNINGHAM SLIP FACTOR FOR A PARTICLE

DIMENSION DIAM(5),KMXFR(7),KP(7)

COMMON/BLK30/DIAM,VP,DIFUS,CM
COMMON/BLK40/TB,VIS,PSPACE
COMMON/BLK5/KMXFR,KP,JMXFR

G=980.
RHOGAS=29.*PSPACE /82.06/TB

C THE FOLLOWING ARE TAKEN FROM THE FOLLOWING REFERENCE:
C OWCZARSKI, P.C., R.I. SHRECK, AND A.K. POSTMA. 1985.
C TECHNICAL BASES AND USER'S MANUAL FOR THE PROTOTYPE OF A
C SUPPRESSION POOL AEROSOL REMOVAL CODE (SPARC).
C NUREG/CR-3317, U.S. NUCLEAR REGULATORY COMMISSION, WASHINGTON D.C.

C ELAM = MEAN FREE PATH OF AIR MOLECULES

PI=3.14159265
ELAM=1.245E-02*((TB/29.)**0.5)*VIS/PSPACE
DPA=DIAM(JMXFR-2)*1.E-04
RATD=ELAM/DPA
CM=1.+2.492*RATD+0.84*RATD*EXP(-0.435/RATD)
DIFUS=4.6E-17*TB*CM/PI/VIS/DPA

C DIFUS IN CM**2./S

VP=1.0*G*CM*DPA**2./18./VIS

FDRE=1.333333*1.0*RHOGAS*G*DPA**3./VIS**2.
IF(FDRE.GT.9.6.AND.FDRE.LT.93.6)RE=(FDRE/27.)**(1./1.13)
IF(FDRE.GE.93.6.AND.FDRE.LT.410.)RE=(FDRE/24.32)**(1./1.227)
IF(FDRE.GE.410..AND.FDRE.LT.1.07E+04)RE=(FDRE/15.71)**(1./1.417)
IF(FDRE.GE.1.07E+04.AND.FDRE.LT.2.4E+05)RE=(FDRE/6.477)
+** (1./1.609)
IF(FDRE.GE.2.4E+05)RE=(FDRE/1.194)**(1./1.867)
IF(FDRE.GT.9.6)VP=RE*VIS/DPA/RHOGAS

C VP IN CM/S

RETURN
END

C*****

SUBROUTINE SPRAY

C THIS SUBROUTINE COMPUTES SPAY WASHOUT OF PARTICLES IN A ROOM DESIGNATED
C AS HAVING SPRAYS (NSPRAY(ISPACE)=1). IT DELIVERS THE PARAMETER LSPRAY(K),
C 1/MIN, TO SUBROUTINE ROOM (K=1,7)

REAL NDROP(5), LSPRAY(7), KP(7), KMXFR(7), LENGTH(20), LSPRY, LSP
DIMENSION DIAM(5), FRAC(5), DROPD(5), FRACD(5)
DIMENSION DSPRAY(20), HSPRAY(20), VSPRAY(20)

DIMENSION CONC(30,7), FP(20,7), FR(30,20), FROUT(30,20),
+FRO(30,20), FRIN(30,20), TNDATA(30), PDATA(30,20), TDATA(30,20),
+NSPACE(20), HEIGHT(20), WIDTH(20), DT(30), VOL(20), AXSXN(20),
+AFLOOR(20), DF1(20), DF2(20), DF3(20), FRI(20), FROUTI(20), FRINI(20),
+TDATAI(20), PDATAI(20), FROI(20), CONCI(7), CPUFF(7), DMULT(20)
DIMENSION CNC(0:19,7,2), CNCP(20,7,2)

COMMON /BLK1/TT,DT,DTT,CNC,CONC,NDATA,NODES,TNDATA,TDATA,PDATA,
+FP,FR,FRO,FROUT,FRIN,NSPACE,HEIGHT,WIDTH,LENGTH,VOL,AXSXN,AFLOOR,
+DF1,DF2,DF3,FROUTI,FRINI,FRI,FROI,PDATAI,TDATAI,CONCI,CNCP

COMMON/BLK3/ISPACE
COMMON/BLK5/KMXFR,KP,JMXFR
COMMON/BLK20/DROPDM,VDROP
COMMON/BLK25/DSPRAY,HSPRAY,VSPRAY
COMMON/BLK30/DIAM,VP,DIFUS,CM
COMMON/BLK40/TB,VIS,PSPACE
COMMON/BLK50/LSPRAY

C NDROP(J), J=1,5, IS THE NUMBER OF SPRAY DROPLETS OF SIZE J IN THE ROOM

C IF(JMXFR.LT.3) LSPRAY(JMXFR)=0.
C NO CREDIT IS GIVEN TO WASHOUT OF NG AND I2.
IF(JMXFR.LT.3) GO TO 100

CALL VISAIR
PI=3.14159265
DATA DROPD/158.489,398.107,1000.,2511.89,6309.57/
DATA FRACD/0.0156896,0.219259,0.530103,0.219259,0.0156896/
C ABOVE DATA STATEMENTS ARE FOR A LOG NORMAL SPRAY DROPLET DISTRIBUTION
C OF MMD=1.0 MILLIMETERS AND GEOMETRIC STANDARD DEVIATION=2..

LSPRY=0.

DO 10 K=1,5

C DROPDM=DROPD(K)*DSPRAY(ISPACE)*1.E-04
C DROPDM IS IN CM
VD=PI*(DROPDM**3.)/6.
CALL VDROPS
TFALL=HSPRAY(ISPACE)*30.48/VDROP

```

NDROP(K)=VSPRAY(ISPACE)*FRACD(K)*TFALL*(3785.412/60.)/VD
CALL PART
JM=JMXFR-2
DP=DIAM(JM)*1.E-04
DD=DROPDM
C THE FOLLOWING IS TAKEN FROM:
C GIESEKE, J.A., P. CYBULSKIS, R.S. DENNING, M.R. KUHLMAN,
C K.W. LEE, AND H. CHEN. 1989. RADIOACTIVE RELEASES UNDER SPECIFIC
C LWR ACCIDENT CONDITIONS, VOL. IV. BMI-2104, BATTELLE MEMORIAL
C INSTITUTE, COLUMBUS OHIO.
C PECLET NUMBER, PE
PE=VDROP*DD/DIFUS
C STOKES NUMBER, STK
STK=DP*DP*1.*VDROP*CM/9./VIS/DD
RAT=DP/DD
C COLLECTION EFFICIENCIES EI, ER, AND ED FOR INERTIAL IMPACTION,
C INTERCEPTION, AND BROWNIAN DIFFUSION, RESPECTIVELY.
EI=STK*STK/(STK+0.35)**2.
ER=1.5*RAT*RAT/(1.+RAT)**0.3333333
ED=3.5/PE**0.6666667
ETOT=EI+ER+ED
DV=VDROP-VP
IF(DV.LT.0.)THEN
  LSPRAY(JMXFR)=0.
  GO TO 100
END IF
VOLISP=28316.85*VOL(ISPACE)
LSP=NDROP(K)*VDROP*ETOT*PI*(DD/2.)**2./VOLISP
LSPRY=LSPRY+LSP
10 CONTINUE
C CONVERT 1/S TO 1/MIN.
LSPRAY(JMXFR)=60.*LSPRY
100 CONTINUE

RETURN
END

```

APPENDIX B

SAMPLE CASE INPUT AND OUTPUT FILES

Section 1: Introduction

The first part of the document discusses the importance of maintaining accurate records and the role of the committee in overseeing these processes.

Section 2: Procedures

The following section outlines the specific procedures to be followed by all members of the organization, including reporting requirements and timelines.

Section 3: Reporting

Members are required to submit reports on a regular basis, detailing their activities and any issues that may arise during their term.

It is the responsibility of the reporting officer to ensure that all information is accurate and up-to-date, and to provide a clear summary of the organization's performance.

Section 4: Financials

The financial section details the budgeting process and the allocation of funds for various organizational activities.

Members should be aware of the financial constraints and work together to ensure that the organization remains within its budget.

Regular financial reviews will be conducted to monitor the organization's financial health and to identify areas for improvement.

The committee will provide guidance and support to members in managing their financial responsibilities effectively.

By following these guidelines, we aim to ensure the transparency and accountability of our organization's operations and to achieve our shared goals.

APPENDIX B

SAMPLE CASE INPUT AND OUTPUT FILES

B.1 COMPLETED BLDINPT2 INPUT FORMS

***** FORM 1 *****

FILENAME TO BE CREATED: FPFP1A.DAT

HEADING FOR FILE (80 CHAR): Sample Puff Release Case

ENTER THE NUMBER OF SPACES: 5

COMPLETE ONE FORM 2 FOR EACH SPACE.

ENTER THE NUMBER OF TIME STEPS FOR DATA INPUT: 3

COMPLETE ONE FORM 3 FOR EACH TIME STEP.

COMPLETE ONE FORM 4 FOR EACH TIME STEP AT EACH NODE.

IS PUFF RELEASE IN SPACE 1 (ROOM) AT TIME(1) (0. MIN) ?: 1=YES 0=NO

ENTER PUFF CONCENTRATIONS IN CORE FRACTIONSS/FT**3
FOR EACH PRODUCT GROUP.

1) 1.000 E-08

2) 1.000 E-08

3) 1.000 E-08

ENTER PARTICLE DIAMETER MULTIPLIER: 1.000

COMPLETE ONE FORM 5 FOR EACH SPACE THAT IS A ROOM.

***** FORM 2 *****

SPACE NUMBER: 1

ENTER NUMBER DESCRIPTION OF SPACE: 1

- 1 = ROOM
- 2 = DUCT
- 3 = FILTER
- 4 = RESISTANCE, e.g. leaky door
- 5 = END DESCRIPTION

IF SPACE IS 1,2,3,4

	HEIGHT	WIDTH	LENGTH
ENTER DIMENSIONS IN FEET:	<u>50</u>	<u>60</u>	<u>100</u>

IF SPACE IS 2

ENTER DUCT ANGLE IN DEGREES: NA

	DF1	DF2	DF3
ENTER DECONTAMINATION FACTOR FOR EACH FISSION PRODUCT GROUP:	<u>1.0</u>	<u>1.0</u>	<u>1.0</u>

***** FORM 2 *****

SPACE NUMBER: 2

ENTER NUMBER DESCRIPTION OF SPACE: 2

- 1 = ROOM
- 2 = DUCT
- 3 = FILTER
- 4 = RESISTANCE, e.g. leaky door
- 5 = END DESCRIPTION

IF SPACE IS 1,2,3,4

	HEIGHT	WIDTH	LENGTH
ENTER DIMENSIONS IN FEET:	<u>10</u>	<u>10</u>	<u>100</u>

IF SPACE IS 2

ENTER DUCT ANGLE IN DEGREES: 45

	DF1	DF2	DF3
ENTER DECONTAMINATION FACTOR FOR EACH FISSION PRODUCT GROUP:	<u>1.0</u>	<u>1.0</u>	<u>1.0</u>

***** FORM 2 *****

SPACE NUMBER: 3

ENTER NUMBER DESCRIPTION OF SPACE: 3

- 1 = ROOM
- 2 = DUCT
- 3 = FILTER
- 4 = RESISTANCE, e.g. leaky door
- 5 = END DESCRIPTION

IF SPACE IS 1,2,3,4

	HEIGHT	WIDTH	LENGTH
ENTER DIMENSIONS IN FEET:	<u>1</u>	<u>1</u>	<u>1</u>

IF SPACE IS 2

ENTER DUCT ANGLE IN DEGREES: NA

	DF1	DF2	DF3
ENTER DECONTAMINATION FACTOR FOR EACH FISSION PRODUCT GROUP:	<u>1.0</u>	<u>20.0</u>	<u>2000.0</u>

***** FORM 2 *****

SPACE NUMBER: 4

ENTER NUMBER DESCRIPTION OF SPACE: 1

- 1 = ROOM
- 2 = DUCT
- 3 = FILTER
- 4 = RESISTANCE, e.g. leaky door
- 5 = END DESCRIPTION

IF SPACE IS 1,2,3,4

	HEIGHT	WIDTH	LENGTH
ENTER DIMENSIONS IN FEET:	<u>12</u>	<u>50</u>	<u>60</u>

IF SPACE IS 2

ENTER DUCT ANGLE IN DEGREES: NA

	DF1	DF2	DF3
ENTER DECONTAMINATION FACTOR FOR EACH FISSION PRODUCT GROUP:	<u>1.0</u>	<u>1.0</u>	<u>1.0</u>

***** FORM 2 *****

SPACE NUMBER: 5

ENTER NUMBER DESCRIPTION OF SPACE: 5

- 1 = ROOM
- 2 = DUCT
- 3 = FILTER
- 4 = RESISTANCE, e.g. leaky door
- 5 = END DESCRIPTION

IF SPACE IS 1,2,3,4

	HEIGHT	WIDTH	LENGTH
ENTER DIMENSIONS IN FEET:	<u>NA</u>	<u>NA</u>	<u>NA</u>

IF SPACE IS 2

ENTER DUCT ANGLE IN DEGREES: NA

ENTER DECONTAMINATION FACTOR	DF1	DF2	DF3
FOR EACH FISSION PRODUCT GROUP:	<u>NA</u>	<u>NA</u>	<u>NA</u>

***** FORM 3 *****

CONCENTRATIONS ENTERING NODE 1.

TIME STEP: 1

ENTER DATA ENTRY TIME (MIN.): 0.0

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 1: 0.0

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 2: 0.0

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 3: 0.0

***** FORM 3 *****

CONCENTRATIONS ENTERING NODE 1.

TIME STEP: 2

ENTER DATA ENTRY TIME (MIN.): 100.0

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 1: 0.0

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 2: 0.0

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 3: 0.0

***** FORM 3 *****

CONCENTRATIONS ENTERING NODE 1.

TIME STEP: 3

ENTER DATA ENTRY TIME (MIN.): 200.0

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 1: 0.0

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 2: 0.0

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 3: 0.0

***** FORM 4 *****

TIME STEP: 1 NODE NUMBER: 1

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 15000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 15000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 4 *****

TIME STEP: 2 NODE NUMBER: 1

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 15000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 15000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 4 *****

TIME STEP: 3 NODE NUMBER: 1

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 15000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 15000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 4 *****

TIME STEP: 1 NODE NUMBER: 2

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 15000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 15000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 4 *****

TIME STEP: 2 NODE NUMBER: 2

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 15000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 15000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 4 *****

TIME STEP: 3 NODE NUMBER: 2

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 15000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 15000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 4 *****

TIME STEP: 1 NODE NUMBER: 3

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 15000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 5000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 10000.0

***** FORM 4 *****

TIME STEP: 2 NODE NUMBER: 3

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 15000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 5000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 10000.0

***** FORM 4 *****

TIME STEP: 3 NODE NUMBER: 3

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 15000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 5000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 10000.0

***** FORM 4 *****

TIME STEP: 1 NODE NUMBER: 4

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 5000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 5000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 4 *****

TIME STEP: 2 NODE NUMBER: 4

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 5000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 5000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 4 *****

TIME STEP: 3 NODE NUMBER: 4

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 5000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 5000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 4 *****

TIME STEP: 1 NODE NUMBER: 5

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 5000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 5000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 4 *****

TIME STEP: 2 NODE NUMBER: 5

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 5000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 5000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 4 *****

TIME STEP: 3 NODE NUMBER: 5

ENTER DOWNSTREAM PRESSURE (PSIG): 0.0

ENTER DOWNSTREAM TEMPERATURE (C): 25.0

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: 5000.0

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : 5000.0

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: 0.0

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: 0.0

***** FORM 5 *****

SPACE NUMBER: _____

DOES ROOM HAVE ACTIVE SPRAYS: 1=YES 0=NO

IF YES

ENTER DROP DIAMETER MULTIPLIER: NA _____

SPRAY FLOW RATE (GPM): NA _____

SPRAY HEIGHT (FT): NA _____

TIME SPRAYS GO ON (MIN): NA _____

TIME SPRAYS GO OFF (MIN): NA _____

***** FORM 5 *****

SPACE NUMBER: _____

DOES ROOM HAVE ACTIVE SPRAYS: 1=YES 0=NO

IF YES

ENTER DROP DIAMETER MULTIPLIER: NA _____

SPRAY FLOW RATE (GPM): NA _____

SPRAY HEIGHT (FT): NA _____

TIME SPRAYS GO ON (MIN): NA _____

TIME SPRAYS GO OFF (MIN): NA _____

B.2 BLDINPT2 GENERATED INPUT FILE

SAMPLE PUFF RELEASE CASE

3	5	1	1.000000	
1.000000E-08	1.000000E-08	1.000000E-08		
0.000000E+00	100.000000	200.000000		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
1	50.000000	60.000000	100.000000	1.000000
1.000000	1.000000			
2	10.000000	10.000000	100.000000	1.000000
1.000000	1.000000			
45.000000				
3	1.000000	1.000000	1.000000	1.000000
20.000000	2000.000000			
1	12.000000	50.000000	60.000000	1.000000
1.000000	1.000000			
15000.000000	15000.000000	15000.000000		
15000.000000	15000.000000	15000.000000		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
25.000000	25.000000	25.000000		
15000.000000	15000.000000	15000.000000		
15000.000000	15000.000000	15000.000000		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
25.000000	25.000000	25.000000		
5000.000000	5000.000000	5000.000000		
15000.000000	15000.000000	15000.000000		
10000.000000	10000.000000	10000.000000		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
25.000000	25.000000	25.000000		
5000.000000	5000.000000	5000.000000		
5000.000000	5000.000000	5000.000000		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
25.000000	25.000000	25.000000		
5000.000000	5000.000000	5000.000000		
5000.000000	5000.000000	5000.000000		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
25.000000	25.000000	25.000000		
5000.000000	5000.000000	5000.000000		
5000.000000	5000.000000	5000.000000		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
0.000000E+00	0.000000E+00	0.000000E+00		
25.000000	25.000000	25.000000		
0				
0				

B.3 PART OF SAMPLE CASE OUTPUT FILE

SAMPLE PUFF RELEASE CASE

```

NODES=      5
NDATA=      3
NPUFF=      1
DMULT=      1.0000
CPUFF(I)=   1.0000E-08   1.0000E-08   1.0000E-08
TNDATA(I)=  0.0000E+00   1.0000E+02   2.0000E+02
K = 1
CONC(K,J)=  0.0000E+00   0.0000E+00   0.0000E+00
K = 2
CONC(K,J)=  0.0000E+00   0.0000E+00   0.0000E+00
K = 3
CONC(K,J)=  0.0000E+00   0.0000E+00   0.0000E+00

```

```

SPACE # K= 1   NSPACE(K)= 1
HEIGHT(K)= 50.000   WIDTH(K)= 60.000   LENGTH(K)= 100.000
DF1(K)= 1.0000E+00   DF2(K)= 1.0000E+00   DF3(K)= 1.0000E+00

```

```

SPACE # K= 2   NSPACE(K)= 2
HEIGHT(K)= 10.000   WIDTH(K)= 10.000   LENGTH(K)= 100.000
DF1(K)= 1.0000E+00   DF2(K)= 1.0000E+00   DF3(K)= 1.0000E+00
SPACE # 2 IS A DUCT, AND HAS AN ANGLE WITH THE HORIZONTAL = 45.00 DEGREES

```

```

SPACE # K= 3   NSPACE(K)= 3
HEIGHT(K)= 1.000   WIDTH(K)= 1.000   LENGTH(K)= 1.000
DF1(K)= 1.0000E+00   DF2(K)= 2.0000E+01   DF3(K)= 2.0000E+03

```

```

SPACE # K= 4   NSPACE(K)= 1
HEIGHT(K)= 12.000   WIDTH(K)= 50.000   LENGTH(K)= 60.000
DF1(K)= 1.0000E+00   DF2(K)= 1.0000E+00   DF3(K)= 1.0000E+00

```

```

NODE 1  NDATA = 1... 3
FR(K,J)= 15000.000   15000.000   15000.000
FRO(K,J)= 15000.000   15000.000   15000.000
FROUT(K,J)= .000   .000   .000
FRIN(K,J)= .000   .000   .000
PDATA(K,J)= .000   .000   .000
TDATA(K,J)= 25.000   25.000   25.000
NODE 2  NDATA = 1... 3
FR(K,J)= 15000.000   15000.000   15000.000
FRO(K,J)= 15000.000   15000.000   15000.000
FROUT(K,J)= .000   .000   .000
FRIN(K,J)= .000   .000   .000
PDATA(K,J)= .000   .000   .000
TDATA(K,J)= 25.000   25.000   25.000
NODE 3  NDATA = 1... 3
FR(K,J)= 5000.000   5000.000   5000.000
FRO(K,J)= 15000.000   15000.000   15000.000
FROUT(K,J)= 10000.000   10000.000   10000.000
FRIN(K,J)= .000   .000   .000

```


PDATA(K,J)=	.000	.000	.000
TDATA(K,J)=	25.000	25.000	25.000
NODE 4 NDATA = 1... 3			
FR(K,J)=	5000.000	5000.000	5000.000
FRO(K,J)=	5000.000	5000.000	5000.000
FROUT(K,J)=	.000	.000	.000
FRIN(K,J)=	.000	.000	.000
PDATA(K,J)=	.000	.000	.000
TDATA(K,J)=	25.000	25.000	25.000
NODE 5 NDATA = 1... 3			
FR(K,J)=	5000.000	5000.000	5000.000
FRO(K,J)=	5000.000	5000.000	5000.000
FROUT(K,J)=	.000	.000	.000
FRIN(K,J)=	.000	.000	.000
PDATA(K,J)=	.000	.000	.000
TDATA(K,J)=	25.000	25.000	25.000

CALCULATED OUTPUT AT .00 MINUTES

CONCENTRATIONS ENTERING NODES, CORE FRACTIONS/FT**3

NOBLE GASES

0.0000E+00	1.0000E-08	0.0000E+00	0.0000E+00	0.0000E+00
------------	------------	------------	------------	------------

IODINE, I2

0.0000E+00	1.0000E-08	0.0000E+00	0.0000E+00	0.0000E+00
------------	------------	------------	------------	------------

PARTICLES

0.0000E+00	1.0000E-08	0.0000E+00	0.0000E+00	0.0000E+00
------------	------------	------------	------------	------------

CONCENTRATIONS LEAVING NODES, CORE FRACTIONS/ FT**3

NOBLE GASES

0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00
------------	------------	------------	------------	------------

IODINE, I2

0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00
------------	------------	------------	------------	------------

PARTICLES

0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00
------------	------------	------------	------------	------------

AVG RATES OF FISSION PRODUCTS LEAVING NODES, CORE FRACTIONS/MIN

NOBLE GASES

0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00
------------	------------	------------	------------	------------

IODINE, I2

0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00
------------	------------	------------	------------	------------

PARTICLES

0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00
------------	------------	------------	------------	------------

CALCULATED OUTPUT AT 10.00 MINUTES

CONCENTRATIONS ENTERING NODES, CORE FRACTIONS/FT**3

NOBLE GASES

0.0000E+00 6.0653E-09 8.0327E-09 4.0163E-09 1.5074E-09

IODINE, I2

0.0000E+00 5.1600E-09 3.9705E-09 9.9263E-11 3.1914E-11

PARTICLES

0.0000E+00 3.8518E-09 2.7656E-09 6.9141E-13 2.0426E-13

CONCENTRATIONS LEAVING NODES, CORE FRACTIONS/ FT**3

NOBLE GASES

0.0000E+00 0.0000E+00 0.0000E+00 0.0000E+00 0.0000E+00

IODINE, I2

0.0000E+00 0.0000E+00 0.0000E+00 0.0000E+00 0.0000E+00

PARTICLES

0.0000E+00 0.0000E+00 0.0000E+00 0.0000E+00 0.0000E+00

AVG RATES OF FISSION PRODUCTS LEAVING NODES, CORE FRACTIONS/MIN

NOBLE GASES

0.0000E+00 1.2049E-04 2.0082E-05 1.0041E-05 3.7686E-06

IODINE, I2

0.0000E+00 1.1370E-04 9.9263E-06 2.4816E-07 7.9784E-08

PARTICLES

0.0000E+00 1.0389E-04 6.9141E-06 1.7285E-09 5.1066E-10

CALCULATED OUTPUT AT 200.00 MINUTES

CONCENTRATIONS ENTERING NODES, CORE FRACTIONS/FT**3

NOBLE GASES

0.0000E+00	4.5400E-13	6.0126E-13	7.9628E-13	1.3442E-12
------------	------------	------------	------------	------------

IODINE, I2

0.0000E+00	1.7904E-14	1.3777E-14	1.0119E-15	1.4033E-15
------------	------------	------------	------------	------------

PARTICLES

0.0000E+00	3.9231E-14	4.5597E-14	3.1125E-17	4.5841E-17
------------	------------	------------	------------	------------

CONCENTRATIONS LEAVING NODES, CORE FRACTIONS/ FT**3

NOBLE GASES

0.0000E+00	9.9131E-13	1.3128E-12	2.2163E-12	0.0000E+00
------------	------------	------------	------------	------------

IODINE, I2

0.0000E+00	2.6700E-14	1.9611E-15	2.7197E-15	0.0000E+00
------------	------------	------------	------------	------------

PARTICLES

0.0000E+00	7.8902E-14	5.3880E-17	7.9237E-17	0.0000E+00
------------	------------	------------	------------	------------

AVG RATES OF FISSION PRODUCTS LEAVING NODES, CORE FRACTIONS/MIN

NOBLE GASES

0.0000E+00	9.0189E-09	3.9814E-09	5.2728E-09	8.9013E-09
------------	------------	------------	------------	------------

IODINE, I2

0.0000E+00	3.9452E-10	1.0119E-10	7.4325E-12	1.0308E-11
------------	------------	------------	------------	------------

PARTICLES

0.0000E+00	8.0432E-10	3.1125E-10	2.1264E-13	3.1282E-13
------------	------------	------------	------------	------------

APPENDIX C

BLANK BLDINPT2 FORMS

APPENDIX C

BLANK BLDINPT2 FORMS

***** FORM 1 *****

FILENAME TO BE CREATED: _____

HEADING FOR FILE (80 CHAR): _____

ENTER THE NUMBER OF SPACES: _____

COMPLETE ONE FORM 2 FOR EACH SPACE.

ENTER THE NUMBER OF TIME STEPS FOR DATA INPUT: _____

COMPLETE ONE FORM 3 FOR EACH TIME STEP.

COMPLETE ONE FORM 4 FOR EACH TIME STEP AT EACH NODE.

IS PUFF RELEASE IN SPACE 1 (ROOM) AT TIME(1) (0. MIN) ?: 1=YES 0=NO

ENTER PUFF CONCENTRATIONS IN CORE FRACTIONSS/FT**3
FOR EACH PRODUCT GROUP.

1) _____

2) _____

3) _____

ENTER PARTICLE DIAMETER MULTIPLIER: _____

COMPLETE ONE FORM 5 FOR EACH SPACE THAT IS A ROOM.

***** FORM 2 *****

SPACE NUMBER: _____

ENTER NUMBER DESCRIPTION OF SPACE: _____

- 1 = ROOM
- 2 = DUCT
- 3 = FILTER
- 4 = RESISTANCE, e.g. leaky door
- 5 = END DESCRIPTION

IF SPACE IS 1,2,3,4

ENTER DIMENSIONS IN FEET: HEIGHT WIDTH LENGTH

IF SPACE IS 2

ENTER DUCT ANGLE IN DEGREES: _____

ENTER DECONTAMINATION FACTOR DF1 DF2 DF3
FOR EACH FISSION PRODUCT GROUP: _____

***** FORM 3 *****

CONCENTRATIONS ENTERING NODE 1.

TIME STEP: _____

ENTER DATA ENTRY TIME (MIN.): _____

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 1: _____

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 2: _____

ENTER CONCENTRATION OF FISSION PRODUCT GROUP 3: _____

***** FORM 4 *****

TIME STEP: _____ NODE NUMBER: _____

ENTER DOWNSTREAM PRESSURE (PSIG): _____

ENTER DOWNSTREAM TEMPERATURE (C): _____

ENTER FLOW (ACFM) INTO NODE N FROM SPACE N-1: _____

ENTER FLOW (ACFM) FROM NODE N TO SPACE N : _____

ENTER FLOW (ACFM) INTO NODE N FROM OUTSIDE FLOW PATH: _____

ENTER FLOW (ACFM) FROM NODE N OUT OF FLOW PATH: _____

***** FORM 5 *****

SPACE NUMBER: _____

DOES ROOM HAVE ACTIVE SPRAYS: 1=YES 0=NO

IF YES

ENTER DROP DIAMETER MULTIPLIER: _____

SPRAY FLOW RATE (GPM): _____

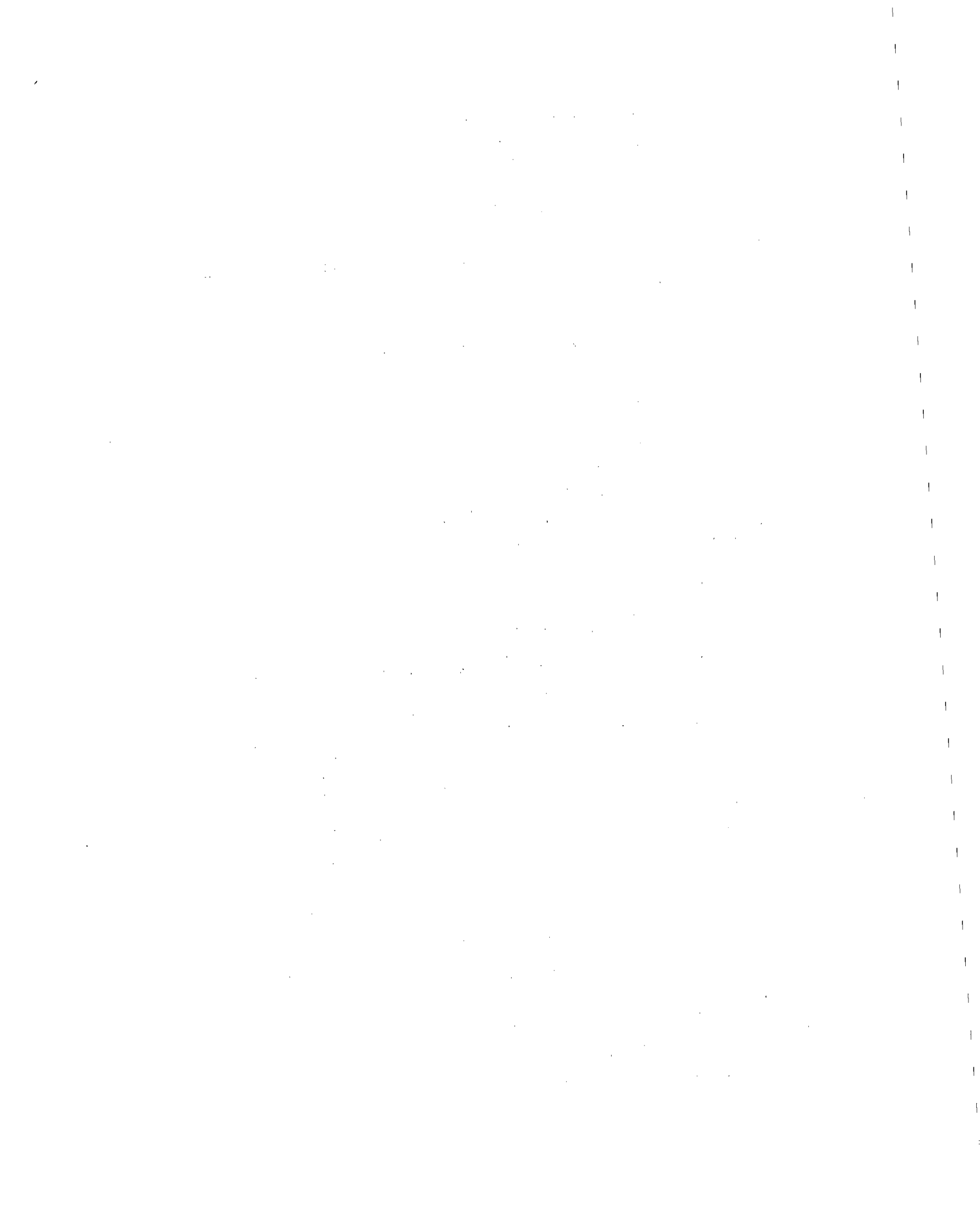
SPRAY HEIGHT (FT): _____

TIME SPRAYS GO ON (MIN): _____

TIME SPRAYS GO OFF (MIN): _____

APPENDIX D

BLDINPT2 LISTING



APPENDIX D

BLDINPT2 LISTING

```

C*****
C
C
C   PROGRAM BLDINPUT
C
C   THIS PROGRAM BUILDS AN INPUT FILE FOR USE BY FPF2_2
C
C
C*****
C   CHARACTER HEAD1*80
C   CHARACTER RESP*1
C
C   REAL LENGTH(20)
C
C   DIMENSION CONC(30,3),FR(30,20),FROUT(30,20),FRO(30,20),
C   .   FRIN(30,20),TNDATA(30),PDATA(30,20),TDATA(30,20),
C   .   NSPACE(20),HEIGHT(20),WIDTH(20),DF1(20),DF2(20),DF3(20),
C   .   cpuff(7),nspray(20),dspray(20),hspray(20),vspray(20),
C   .   tson(20),tsoff(20),THETA(20)
C
C   CHARACTER*12 OUTFILE,NEWFILE
C   CHARACTER*10 STYPE(4)
C
C   DATA STYPE / '   ROOM','   DUCT','   FILTER','RESISTANCE'/
C
C   WRITE(*,1)
C 1 FORMAT(/' Program Title:  FPF2. '//
C   + '   Developed For:   U.S. Nuclear Regulatory Commission'//
C   + '                   Office of Nuclear Regulatory Research'//
C   + '                   Division of Reactor Accident Analysis'//
C   + '   Date:           June 1990'//
C   + '   NRC Contact(s): C. Ferrell           Phone: (FTS) 492-3944'//
C   + '   Code Developer: P. C. Owczarcki     Phone: (509) 376-1701'//
C   + '                   (FTS) 444-1701'//
C   + '   Code Documentation: '//
C   + '   The program was prepared for an agency of the United States',
C   + '   Government. Neither'// the United States Government nor any',
C   + '   agency thereof, nor any of their'// employees, makes any',
C   + '   warranty, expressed or implied, or assumes any legal'//
C   + '   liability or responsibilities for any third party's use,',
C   + '   or the results of such'// use, of any portion of this',
C   + '   program or represents that its use by such third'// party',
C   + '   would not infringe privately owned rights. '// )

```

```

WRITE(*,2)
2  FORMAT(1X,'Press RETURN to Continue')
   READ(5,'(A)')RESP

WRITE(*,'(/A)') ' *****'
WRITE(*,'(A)')  ' ***** PROGRAM BLDINPUT *****'
WRITE(*,'(A)')  ' ***** AN INTERACTIVE PROGRAM *****'
WRITE(*,'(A)')  ' ***** TO CREATE AN INPUT FILE *****'
WRITE(*,'(A)')  ' ***** FOR PROGRAM FPFP *****'
WRITE(*,'(A)')  ' *****'

WRITE(*,600)
600 FORMAT(//,' ENTER THE FILENAME TO BE CREATED > ', $)
    READ(*,'(A)')OUTFILE
699 OPEN(UNIT=1,FILE=OUTFILE,STATUS='NEW',IOSTAT=IER)
    IF(IER .EQ. 6415) THEN
        WRITE(*,601)OUTFILE
601  FORMAT(/,5X,'* * * ',A12,' ALREADY EXISTS * * *',/)
        WRITE(*,602)
602  FORMAT(' ENTER A NEW FILENAME, ',
*      ' OR HIT <RETURN> TO OVERWRITE OLD FILE > ', $)
        READ(*,'(A)')NEWFILE
        IF(NEWFILE(1:3) .EQ. ' ') THEN
            WRITE(*,603)OUTFILE
603  FORMAT(/,5X,A12,' WILL BE OVERWRITTEN',/)
            OPEN(UNIT=1,FILE=OUTFILE,STATUS='UNKNOWN')
        ELSE
            WRITE(*,604)NEWFILE
604  FORMAT(/,5X,A12,' WILL BE OPENED',/)
            OUTFILE = NEWFILE
            GOTO 699
        ENDIF
    ENDIF

10 WRITE(*,'(/A)') ' ENTER A HEADING -- 80 CHARACTERS MAXIMUM '
   READ(*,'(A)',ERR=10) HEAD1
   WRITE(*,'(A)') HEAD1
   WRITE(1,'(A)') HEAD1

C  BUILD FLOW PATH

   WRITE(*,'(/A)') ' DESCRIBE FLOW PATH '

   NODES = 1

100 CONTINUE

WRITE(*,'(/A,12)') ' ENTER NUMBER DESCRIPTION OF SPACE ', NODES
WRITE(*,'(A)')      ' 1 == ROOM'
WRITE(*,'(A)')      ' 2 == DUCT'
WRITE(*,'(A)')      ' 3 == FILTER'
WRITE(*,'(A)')      ' 4 == RESISTANCE, e.g. leaky door'

```

```

IF( NODES .GT. 1 )
  WRITE(*,'(A)') ' 5 == DONE WITH DESCRIPTION'
  READ(*,'(BN,I2)',ERR=100) KOPT

```

```

IF( KOPT .LT. 1 .OR. KOPT .GT. 5 ) THEN
  GOTO 100

```

```

ELSE IF ( KOPT .NE. 5 ) THEN
  WRITE(*,'(A,I2,A,A)') ' SPACE',NODES,' IS A ',STYPE(KOPT)
  NSPACE(NODES) = KOPT
110 WRITE(*,'(A,A,I2,/A)') ' ENTER HEIGHT, WIDTH AND LENGTH IN FT'
  ' FOR SPACE ',NODES,' SEPARATED BY COMMAS'
  READ(*,'(BN,3F10.0)',ERR=110) HEIGHT(NODES),WIDTH(NODES),
  ' LENGTH(NODES)
  WRITE(*,'(5X,3(A,1PE10.2))') 'HEIGHT =',HEIGHT(NODES),' WIDTH ='
  ' WIDTH(NODES), ' LENGTH =', LENGTH(NODES)
  IF(KOPT .EQ. 2) THEN
    WRITE(*,'(/,A,A,I2,/A,A)') ' ENTER ANGLE OF DUCT WITH',
    ' HORIZONTAL FOR SPACE ',NODES,'. ENTER ANGLE',
    ' IN DEGREES, 0 = HORIZONTAL'
    READ(*,'(F8.0)')THETA(NODES)
    WRITE(*,'(5X,A,1PE10.2)') 'DUCT ANGLE = ',THETA(NODES)
  ENDIF

```

C SET DECONTAMINATION FACTORS FOR SPACE

```

IF( KOPT .NE. 3 ) THEN
  DF1(NODES) = 1.0
  DF2(NODES) = 1.0
  DF3(NODES) = 1.0
ELSE
120 WRITE(*,'(A,A,/A)') ' ENTER DECONTAMINATION FACTOR FOR EACH'
  ' FISSION PRODUCT GROUP -- ', ' SEPARATED BY COMMAS'
  READ(*,'(BN,3F10.0)',ERR=120) DF1(NODES),DF2(NODES),DF3(NODES)
  WRITE(*,'(A,3F10.1)') ' DECONTAMINATION FACTORS ARE:',
  ' DF1(NODES), DF2(NODES), DF3(NODES)
ENDIF

```

```

NODES = NODES + 1
IF( NODES .LT. 21 ) THEN
  GOTO 100

```

```

ELSE
  WRITE(*,'(//A)') ' TOO MANY SPACES '
  STOP
ENDIF
ENDIF

```

C ENTER TIMES AND CONCENTRATIONS AT THE INITIAL FLOW PATH NODE

```

200 WRITE(*,'(/A,A)') ' ENTER THE NUMBER OF TIME STEPS FOR DATA INPUT',
  ' , MAX = 30 '
  READ(*,'(BN,I4)',ERR=200) NDATA
  WRITE(*,'(2X,I4,A)') NDATA,' DATA ENTRY TIMES '

```

```

WRITE(*, '(/A,A)') ** ENTER TIME AND CORRESPONDING ',
'CONCENTRATIONS AT INITIAL FLOW PATH NODE **'

DO 240 I = 1, NDATA
210 WRITE(*, '(/A,I3)') ' ENTER DATA ENTRY TIME IN MIN ', I
READ(*, '(BN,F10.0)', ERR=210) TNDATA(I)
WRITE(*, '(A,I2,A,F7.1)') ' DATA ENTRY TIME ', I, ' = ', TNDATA(I)

DO 230 J = 1, 3
220 WRITE(*, '(A,A,I2,A)') ' ENTER CONCENTRATION OF FISSION',
' PRODUCT GROUP ', J, ' IN CORE FRACTION/FT**3'
READ(*, '(BN,F15.0)', ERR=220) CONC(I,J)
WRITE(*, '(A,I2,A,1PE10.2)') ' FISSION PRODUCT GROUP', J,
' CONCENTRATION = ', CONC(I,J)
230 CONTINUE
240 CONTINUE

C DEFINE FLOWS, PRESSURES AND TEMPERATURES AT NODES AS FUNCTIONS
C OF TIME

WRITE(*, '(A,A)') ' DEFINE PRESSURES, TEMPERATURES AND FLOWS AT ',
' NODES AS FUNCTIONS OF TIME'

DO 370 I = 1, NODES
DO 360 J = 1, NDATA

WRITE(*, '(/A,I2,A,F7.1)') ' NODE = ', I, ' TIME = ', TNDATA(J)
300 WRITE(*, '(A)') ' ENTER DOWNSTREAM PRESSURE, PSIG '
READ(*, '(BN,F10.0)', ERR=300) PDATA(J,I)
310 WRITE(*, '(A)') ' ENTER DOWNSTREAM TEMPERATURE, C'
READ(*, '(BN,F10.0)', ERR=310) TDATA(J,I)
320 WRITE(*, '(A,I2,A,I2)') ' ENTER FLOW (ACFM) INTO NODE ', I,
' FROM SPACE ', I-1
READ(*, '(BN,F10.0)', ERR=320) FRO(J,I)
330 WRITE(*, '(A,I2,A,I2)') ' ENTER FLOW (ACFM) FROM NODE ', I,
' TO SPACE ', I
READ(*, '(BN,F10.0)', ERR=330) FR(J,I)
340 WRITE(*, '(A,I2,A)') ' ENTER FLOW (ACFM) INTO NODE ', I,
' FROM OUTSIDE FLOW PATH'
READ(*, '(BN,F10.0)', ERR=340) FRIN(J,I)
350 WRITE(*, '(A,I2,A)') ' ENTER FLOW (ACFM) FROM NODE ', I,
' OUT OF FLOW PATH'
READ(*, '(BN,F10.0)', ERR=350) FROUT(J,I)
WRITE(*, '(A,/6(1PE12.2))') ' PRESSURE, TEMPERATURE & FLOWS',
PDATA(J,I), TDATA(J,I), FRO(J,I), FR(J,I), FRIN(J,I),
FROUT(J,I)

360 CONTINUE
370 CONTINUE

```



```

c   DEFINE PUFF RELEASE

380 write(*, '(/a,a)') ' PUFF RELEASE IN SPACE 1 = ROOM AT',
    ' TNDATA(1)=0.? YES = 1, NO = 0'
    read(*, '(bn,i4)',ERR=381) npuff
381 IF(NPUFF .NE. 1 .AND. NPUFF .NE. 0) GOTO 380

500 write(*, '(a,a,a)') ' ENTER PUFF CONCENTRATIONS IN',
    ' CORE FRACTIONSS/FT**3 FOR EACH PRODUCT GROUP.',
    ' SEPARATE BY COMMAS.'
    read(*, '(bn,3f10.0)',err=500)(cpuff(i),i=1,3)
540 continue

c   DEFINE PARTICLE DIAMETER MULTIPLIER

550 write(*, '(a)') ' ENTER PARTICLE DIAMETER MULTIPLIER'
    read(*, '(bn,f10.0)',err=550)dmult

c   DEFINE SPRAY USAGE

    do 400 i=1,nodes-1
    if(nspace(i).ne.1) go to 390
430 write(*, '(a,i2,a)') ' DOES SPACE('I,') HAVE ACTIVE SPRAYS?'
    write(*, '(a)') ' ENTER 1 IF YES, 0 IF NO'
    read(*, '(bn,i4)',err=430) nspray(i)
    if(nspray(i).ne.1)go to 390
440 write(*, '(a,/a,/a,/a)') ' ENTER DROP DIAM MULTIPLIER; SPRAY FLOW
    .RATE, GPM; SPRAY HEIGHT, FT', 'TIME SPRAYS GO ON, MIN; AND
    .TIME SPRAYS GO OFF, MIN.', ' SEPARATE BY COMMAS.'
    read(*, '(bn,5f10.0)',err=440)dspray(i),vspray(i),hspray(i),
    .tson(i),tsoff(i)
390 continue
400 continue

C   WRITE DATA TO FILE FPPF_2.DAT

WRITE(1,*) NDATA,NODES,npuff,dmult
if(npuff.eq.1)then
  write(1,*)(cpuff(i),i=1,3)
end if
WRITE(1,*) (TNDATA(I), I=1,NDATA)

DO 405 K=1,NDATA
  WRITE(1,*)(CONC(K,J),J=1,3)
405 CONTINUE

DO 410 K=1,NODES-1
  WRITE(1,*)NSPACE(K),HEIGHT(K),WIDTH(K),LENGTH(K),DF1(K),DF2(K),
+ DF3(K)
  IF(NSPACE(K) .EQ. 2) WRITE(1,*)THETA(K)
410 CONTINUE

```

```
DO 420 J=1, NODES
  WRITE(1, *) (FR(K, J), K=1, NDATA)
  WRITE(1, *) (FRO(K, J), K=1, NDATA)
  WRITE(1, *) (FROUT(K, J), K=1, NDATA)
  WRITE(1, *) (FRIN(K, J), K=1, NDATA)
  WRITE(1, *) (PDATA(K, J), K=1, NDATA)
  WRITE(1, *) (TDATA(K, J), K=1, NDATA)
420 CONTINUE

do 450 k=1, nodes-1
  if(nspace(k).eq.1)write(1,*)nspray(k)
  if(nspray(k).ne.1)go to 445
  write(1,*)dspray(k),hspray(k),vspray(k),tson(k),tsoff(k)
445 continue
450 continue

RETURN
END
```

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